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Particle pressure and marginal stability limits for a homogeneous monodisperse gas-fluidized bed: kinetic theory and numerical simulations

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A linear stability analysis is performed for the homogeneous state of a monodisperse gas-fluidized bed of spherical particles undergoing hydrodynamic interactions and solid-body collisions at small particle Reynolds number and finite Stokes number. A prerequisite for the stability analysis is the determination of the particle velocity variance which controls the particle-phase pressure. In the absence of an imposed shear, this velocity variance arises solely due to the hydrodynamic interactions among the particles. Since the uniform state of these suspensions is unstable over a wide range of values of particle volume fraction ϕ and Stokes number St , full dynamic simulations cannot be used in general to characterize the properties of the homogeneous state. Instead, we use an asymptotic analysis for large Stokes numbers together with numerical simulations of the hydrodynamic interactions among particles with specified velocities to determine the hydrodynamic sources and sinks of particle-phase energy. In this limit, the velocity distribution to leading order is Maxwellian and therefore standard kinetic theories for granular/hard-sphere molecular systems can be used to predict the particle-phase pressure and rheology of the bed once the velocity variance of the particles is determined. The analysis is then extended to moderately large Stokes numbers for which the anisotropy of the velocity distribution is considerable by using a kinetic theory which combines the theoretical analysis of Koch (1990) for dilute suspensions ($\phi \ll 1$) with numerical simulation results for non-dilute suspensions at large Stokes numbers. A linear stability analysis of the resulting equations of motion provides the first *a priori* predictions of the marginal stability limits for the homogeneous state of a gas-fluidized bed. Dynamical simulations following the detailed motions of the particles in small periodic unit cells confirm the theoretical predictions for the particle velocity variance. Simulations using larger unit cells exhibit an inhomogeneous structure consistent with the predicted instability of the homogeneous gas–solid suspension.

1. Introduction

One of the simplest and yet most stringent challenges in the modelling of gas–particulate flows is to predict the conditions under which a homogeneous fluidized bed will be unstable to volume fraction variations. Jackson (1963) showed that equations of motion which include particle-phase inertia and a drag coefficient that is a function of volume fraction lead to a prediction that the bed will always be unstable. This

instability arises because the volume-fraction-dependent drag yields a kinematic wave speed that differs from the mean velocity of the particles. Therefore, volume-fraction waves propagate relative to a test particle and lead to a time-dependent drag force acting on the particle. The particle's inertia causes it to overshoot this forcing and move toward regions of higher volume fractions. Later studies (Anderson & Jackson 1968) introduced the concept of a particulate-phase pressure that tends to resist variations in volume fraction and thereby has a stabilizing influence. By a suitable choice of the particle pressure as a function of solids volume fraction it was possible to explain the stability of fluidized beds. However, the resulting theory is not predictive in the absence of a method of calculating the particle pressure from first principles. Batchelor (1988) suggested that the particle pressure be related to the hydrodynamic particle self-diffusivity in a low Reynolds number liquid–solid suspension and used measurements and plausible reasoning concerning this quantity to suggest a model for the particle pressure. While this suggestion has some physical basis, it ignores inertial effects and is most applicable to low-to-moderate Reynolds number liquid–fluidized beds. More recent studies (Didwania & Homsy 1982; Anderson, Sundaresan & Jackson 1995; Glasser, Kevrekidis & Sundaresan 1997; Goz 1995; Harris & Crighton 1994; Batchelor 1993) have explored the complex dynamics that occur beyond the onset of the initial instability without seriously re-examining the assumed form of equations of motion.

Recent progress in the kinetic theory of granular materials and theories and numerical simulations of gas–solid suspensions raises the prospect that the particle pressure may be derived from first principles allowing an *a priori* determination of the marginal stability limits for a monodisperse fluidized bed. The kinetic theory of granular materials or dense gases (Lun *et al.* 1984; Jenkins & Richman 1985) shows that a particle pressure arises when momentum is transported by the random translational motion of the particles and when interparticle collisions instantaneously transport momentum from the centre of one particle to another. A crucial step in determining the particle pressure is to predict the magnitude of the particle velocity fluctuations. In the theory of rapid granular flows, the particle temperature (or one-third the velocity variance) is determined by a balance of the work done to shear the fluid with the energy dissipated by inelastic interparticle collisions.

Sangani *et al.* (1996) incorporated the effects of the interstitial gas in a study of rapid shearing motion of a particulate suspension. Exploiting the large $O(2000)$ ratio of the particle to gas density, the inertia of the particles was retained while the inertia of the gas was neglected. The viscous dissipation due to the interstitial flow supplemented the dissipation due to inelastic collisions lowering the particle temperature relative to that for particles in vacuum. The rate of dissipation was determined from a simulation for a suspension of particles with a Maxwellian velocity distribution. A kinetic theory which incorporated this viscous dissipation rate was able to predict most of the rheological properties observed in full dynamic simulations of sheared suspensions with hydrodynamic interactions among the particles.

In a homogeneous fluidized bed, there is no shearing motion to provide the source in the fluctuation energy budget for the particulate phase. Koch (1990) noted that an alternative source of energy could arise from the random forces acting on a particle due to the hydrodynamic disturbances produced by its neighbours as they settle relative to the gas. Koch determined the magnitude of this source in dilute suspensions, $\phi \ll 1$, of very ($St \gg \phi^{-3/2}$) massive particles for which the mean-free time between collisions is smaller than the particle viscous relaxation time $m/(6\pi\mu a)$ and moderately ($\phi^{-3/2} \gg St \gg \phi^{-3/4}$) massive particles for which the

viscous relaxation time is shorter than the collision time. Here, ϕ is the particle volume fraction, $St = mU_t/(6\pi\mu a^2)$ is the Stokes number, m and a are the mass and radius of the particles, $U_t = mg/(6\pi\mu a)$ is the terminal velocity of an isolated particle, g is the acceleration due to gravity, and μ is the gas viscosity. Using this source to determine the particle temperature and pressure, Koch considered the limits of stability for a dilute sedimenting gas–solid suspension. A region of stability was predicted but only for very dilute suspensions $\phi \leq O(St^{-2/3})$.

In this paper, Koch's (1990) theoretical predictions for the particle pressure and the marginal stability limits will be extended to higher particle volume fractions. At high Stokes numbers the source of energy is related to a time integral of the autocorrelation of the force felt by a test particle. Since the homogeneous fluidized state is generally unstable, this correlation cannot be determined by straightforward dynamic simulation of the particles' motion in a gas. We exploit the fact that in this limit the velocities of all the particles are nearly equal with the distribution of the small velocity fluctuation being nearly Maxwellian. The autocorrelation of the force can therefore be evaluated by computing the force on the particles having the same speed but moving according to a hard-sphere Maxwellian distribution. In §2 we use a method of multipole expansion described in Mo & Sangani (1994) and Sangani & Mo (1996) for computing the force on the particles given their velocities to determine the force autocorrelation and hence the source of velocity fluctuations for ϕ ranging from 0.03 to about 0.56.

In §3, we develop a kinetic theory for concentrated suspensions of moderate-Stokes-number particles whose velocity variance is significantly anisotropic. Koch (1990) determined the anisotropic source in this regime for dilute suspensions where the collisional distribution of fluctuation energy into vertical and horizontal velocity moments is negligible. We modify his analysis to account for the collisional redistribution of energy and the effect of particle interactions at finite ϕ on the source of energy.

Knowing the velocity variance, granular flow theory may be used to determine the particle-phase pressure and rheology. The resulting set of equations for the particle phase is analysed in §4 to determine the criterion for the stability of homogeneous fluidized suspensions to small perturbations. It is found that these suspensions are unstable over a wide range of values of ϕ and St . While this is generally well known, it must be appreciated that the present study is the first one based on equations of motion in which all the important terms are derived from first principles.

Section 5 presents the results of dynamic simulations following the motion of individual particles. We first consider relatively dilute suspensions with a small system size for which we expect the suspension to be stable. The simulations for this case allow us to validate the theory for velocity variance over a wide range of Stokes numbers. Next, we consider more concentrated suspensions where the suspension is expected to be unstable even for small system sizes. Our simulations show clear evidence for the instabilities arising in these dense suspensions.

2. Particle velocity variance in a homogeneous suspension

We begin our analysis with the derivation of a general expression for the source of fluctuation energy in a homogeneous suspension. The velocity of a representative particle α sedimenting through a gas satisfies

$$m \frac{d\mathbf{v}^\alpha}{dt} = m\mathbf{g} + \mathbf{F}_v^\alpha + \mathbf{F}_c^\alpha, \quad (1)$$

where m is the mass of the particle, \mathbf{g} is the gravitational acceleration, \mathbf{F}_v^α is the force resulting from the viscous stresses in the gas around the particle, and \mathbf{F}_c^α is the collision force experienced by the particle when it comes in contact with another particle in the suspension. Note that the buoyancy force is neglected in the above expression since the density of the gas is typically much smaller than the density of the particle. The viscous force will in general depend on the velocity and position of all the particles in the suspension. We shall denote the average over all the particles in the suspension by an angular bracket. Since the sum of the collisional forces on the colliding particles vanishes, averaging (1) yields

$$m \frac{d\langle \mathbf{v} \rangle}{dt} = m\mathbf{g} + \langle \mathbf{F}_v \rangle. \quad (2)$$

Note that the above applies strictly to homogeneous suspensions for which the spatial gradients in the average velocity and volume fraction vanish. The spatial derivative terms to account for slow variations in these quantities will be added to the above equation later in §4 where we consider the stability of homogeneous suspensions to small spatial gradients of particle volume fraction.

An equation for the fluctuation energy in homogeneous suspensions can be obtained now by multiplying (1) by \mathbf{v}^α and subtracting from its average an equation obtained by multiplying (2) by $\langle \mathbf{v} \rangle$. This yields

$$\frac{3m}{2} \frac{dT}{dt} = \langle \mathbf{v}^\alpha \cdot (\mathbf{F}_v^\alpha + \mathbf{F}_c^\alpha) \rangle - \langle \mathbf{v} \rangle \cdot \langle \mathbf{F}_v \rangle, \quad (3)$$

where $T = (\frac{1}{3})(\langle v^{\alpha 2} \rangle - \langle v \rangle^2)$ is the particle-phase temperature. At steady state the terms on both sides of the above equation must vanish for homogenous suspensions. It is convenient, to decompose the right-hand side into a number of terms representing the sources and sinks of fluctuation energy by various mechanisms. For example, in rapidly sheared gas–solid suspensions examined in Sangani *et al.* (1996), and in the rapid granular flow literature (e.g. Lun *et al.* 1984), the source of energy is expressed in terms of a product of the particle-phase stress and the strain rate while the sink is expressed in terms of energy dissipation by viscous forces acting on the particles and due to inelastic collisions. Expressing the right-hand side of (3) by $S - \Gamma$ with Γ representing the sink of energy that occurs in the absence of shearing motion and relative motion between the phases, we obtain an expression for the source of energy fluctuations as

$$S = \Gamma + \langle \mathbf{v}^\alpha \cdot (\mathbf{F}_v^\alpha + \mathbf{F}_c^\alpha) \rangle - \langle \mathbf{v} \rangle \cdot \langle \mathbf{F}_v \rangle. \quad (4)$$

The dissipation rate is $\Gamma = \Gamma_{\text{vis}} + \Gamma_{\text{inelas}}$ with the viscous and inelastic sinks given, respectively, by (Sangani *et al.* 1996)

$$\Gamma_{\text{vis}} = 18\pi\mu Ta R_{\text{diss}}(\phi), \quad (5)$$

$$\Gamma_{\text{inelas}} = \frac{12m}{a\pi^{1/2}}(1-e)\phi\chi T^{3/2}, \quad (6)$$

where χ is the value of the radial distribution function at contact. (Note that Γ in the present paper is equivalent to Γ/n in the notation of Sangani *et al.* 1996.) The above two expressions correspond to the energy dissipation per particle in a suspension with an isotropic Maxwellian velocity distribution with a zero mean velocity and $3T$ variance when the Reynolds number based on particle radius a and characteristic fluctuation velocity $T^{1/2}$ is small compared with unity and when e , the coefficient of restitution for particle collisions, is close to unity (nearly elastic collisions). $R_{\text{diss}}(\phi)$

accounts for the particle interactions in Stokes flow. Expressions for this quantity and χ will be given later in this section.

With Γ specified, one can, in principle, compute S from dynamic simulations of sedimenting particles by evaluating the right-hand side of (4) using the force and velocity of each particle computed at every time step in simulations. This procedure is suitable provided that the suspension remains homogeneous. Since we are primarily interested in investigating the stability of the homogeneous state itself, this procedure cannot be adopted. It also does not allow one to develop a simple analytical expression for the source of energy as a function of Stokes number and other relevant variables. Therefore, we shall use a perturbation technique to determine S in the limit of large Stokes number for nearly elastic particles. An approximate theory will then be developed for the case of moderate Stokes numbers.

2.1. Suspensions of high-Stokes-number, nearly elastic particles

In a high-Stokes-number suspension, the particles respond only weakly to hydrodynamic velocity disturbances in the gas. Since these hydrodynamic interactions are the only source of velocity variance in a monodisperse, sedimenting suspension, the leading-order approximation to the particle velocity is simply a common mean velocity $\mathbf{U} = \langle \mathbf{v} \rangle$ obtained by solving (2). Koch (1990) showed that the particle velocities in a high-Stokes-number sedimenting suspension of perfectly elastic particles can be expanded in inverse powers of $St^{-1/3}$. Therefore, we expand the velocity of a particle in a series

$$\mathbf{v}^\alpha = \mathbf{U} + \mathbf{v}_{II}^\alpha + \mathbf{v}_{III}^\alpha + \dots \quad (7)$$

where $U \gg v_{II} \gg v_{III} \dots$, $\mathbf{0} = \langle \mathbf{v}_{II} \rangle = \langle \mathbf{v}_{III} \rangle \dots$. It will be shown that, for large St and $e = 1$, v_{II}/U and v_{III}/v_{II} are $O(St^{-1/3})$. Similarly, we expand the viscous and collisional forces on particle α in a series

$$\mathbf{F}_v^\alpha = \mathbf{F}_{v,I}^\alpha + \mathbf{F}_{v,II}^\alpha + \mathbf{F}_{v,III}^\alpha + \dots \quad (8)$$

Here, $\mathbf{F}_{v,I}^\alpha$ represents the viscous force on particle α when all the particles are moving with the velocity \mathbf{U} , $\mathbf{F}_{v,II}^\alpha$ the force on the particle given the velocity of particle γ to be \mathbf{v}_{II}^γ , $\gamma = 1, 2, \dots, N$, N being the number of particles in the suspension, and so on. Once again, $F_{v,II}/F_{v,I}$ and $F_{v,III}/F_{v,II}$ are expected to be of $O(St^{-1/3})$ for elastic particles.

The mean velocity is controlled by a balance of the gravitational and drag forces acting on the particles as well as the particle inertia in cases of unsteady flows. Since the particles have a common velocity, this leading-order velocity does not contribute to the collisional force. The mean velocity is obtained from the average momentum balance for the particles (2).

The characteristic value of the collisional force $\mathbf{F}_{c,II}^\alpha$ averaged over a small time interval is mv_{II}^2/a since the change in momentum upon a collision is $O(mv_{II})$ and the collision frequency is $O(v_{II}/a)$. Thus, the velocity fluctuations \mathbf{v}_{II}^γ induce collisional contributions to the momentum balance that are $O(\mu a U St^{1/3})$ and the leading approximation to the momentum balance is

$$m \frac{d\mathbf{v}_{II}^\alpha}{dt} = \mathbf{F}_{c,II}^\alpha. \quad (9)$$

The viscous and gravity forces do not contribute to the above equation of motion indicating that to leading order the particle fluctuation velocity is similar to that of a hard-sphere molecular system. Together with the condition $\langle \mathbf{v}_{II}^\alpha \rangle = 0$, (9) implies that

the velocity distribution $f(\mathbf{v}_{II})$ is an isotropic Maxwellian. If we further require that the variance in v^α be the same as the variance in v_{II}^α , we have

$$f(\mathbf{v}_{II}) = \frac{1}{(2\pi T)^{3/2}} \exp\left(-\frac{v_{II}^2}{2T}\right), \quad (10)$$

where T is the granular temperature.

Although the leading-order momentum balance (9) establishes that the particle velocity distribution is nearly Maxwellian, it is not sufficient for determining the granular temperature T . This is because (9) includes only conservative forces. The $O(\mu a U)$ contributions to the momentum balance (1) are

$$m \frac{d\mathbf{v}_{III}^\alpha}{dt} = -\langle \mathbf{F}_{v,I} \rangle + \mathbf{F}_{v,I}^\alpha + \mathbf{F}_{c,III}^\alpha, \quad (11)$$

where we have used the result $-m\mathbf{g} = \langle \mathbf{F}_{v,I} + \mathbf{F}_{v,II} + \mathbf{F}_{v,III} + \dots \rangle$ obtained by applying (2) at steady state. The collisional force $\mathbf{F}_{c,III}^\alpha = O(\mu a U)$, because it results from $O(mv_{III}^\alpha) = O(mU/St^{2/3})$ changes in momentum which occur at an $O(v_{II}/a) = O(US t^{-1/3}/a)$ rate. The correction \mathbf{v}_{III} to the Maxwellian velocity is driven by $\mathbf{F}_{v,I}^\alpha - \langle \mathbf{F}_{v,I} \rangle$, which represents the fluctuation in the force driven by the mean velocity \mathbf{U} of the particles. This force fluctuates because of variations in the spatial configuration of the particles. In a dynamic suspension, $\mathbf{F}_{v,I}^\alpha - \langle \mathbf{F}_{v,I} \rangle$ will vary with time as a particle translates relative to its neighbours.

To summarize, the particle velocity \mathbf{v}^α consists to leading-order of a common mean velocity \mathbf{U} , which may be determined by the mean momentum balance for the particle phase (2). The $O(US t^{-1/3})$ correction to this velocity has a Maxwellian distribution, because the leading-order momentum balance (9) for the individual particles is dominated by elastic interparticle collisions. Finally, an $O(US t^{-2/3})$ correction is driven by the fluctuating viscous force associated with the gas flow induced by the mean motion of the particle assembly motion. This fluctuating force changes with time as the particles move relative to one another with a motion that can be approximated using hard-sphere dynamics.

To see how \mathbf{v}_{III} determines the granular temperature of the suspension, we must examine the energy balance of the particle phase (3). The right-hand side of (3) is given to leading order by

$$\langle \mathbf{v}_{II}^\alpha \cdot (\mathbf{F}_{v,II}^\alpha + \mathbf{F}_{c,II}^\alpha) \rangle + \langle \mathbf{v}_{III}^\alpha \cdot (\mathbf{F}_{v,I}^\alpha - \langle \mathbf{F}_{v,I} \rangle) \rangle, \quad (12)$$

where we have used the fact that \mathbf{v}_{II}^α is uncorrelated with the particles' spatial configuration and, hence, with $\mathbf{F}_{v,I}^\alpha$. The first term in the above expression simply represents the energy dissipation per particle in a suspension with the particle velocities given by an isotropic Maxwellian, and therefore represents $-\Gamma$ (cf. (5) and (6)). Comparing the above with (4), we see that to leading order the source of energy fluctuation is given by

$$S = \langle \mathbf{v}_{III}^\alpha \cdot \hat{\mathbf{F}}_{v,I}^\alpha \rangle, \quad (13)$$

where $\hat{\mathbf{F}}_{v,I}^\alpha = \mathbf{F}_{v,I}^\alpha - \langle \mathbf{F}_{v,I} \rangle$ and \mathbf{v}_{III}^α can be obtained by integrating (11) over time. Denoting the right-hand side of (11) by \mathbf{F}^α , the above expression for the source can be expressed as

$$S = m^{-1} \left\langle \hat{\mathbf{F}}_{v,I}^\alpha(t) \cdot \int_{-\infty}^t \hat{\mathbf{F}}^\alpha dt \right\rangle. \quad (14)$$

Thus, we see that the source is related to the autocorrelation of the force felt by

a representative particle. We expect the correlation time to be comparable with the $O(a/T^{1/2})$ time over which the spatial configuration of particles changes significantly. We therefore write the source as the product of the square of the $O(6\pi\mu aU)$ force and the $O(a/T^{1/2})$ correlation time scale, i.e.

$$S = \frac{a(6\pi\mu a)^2 U^2}{mT^{1/2}} S^*(\phi). \quad (15)$$

In deriving (15), we have assumed that the average velocity of the gas–solid mixture is zero. However, this expression may be generalized to non-zero mixture velocities by replacing U by the relative velocity of the two phases. S^* is the non-dimensional source which will be determined using numerical simulations in §2.2.

In summary, the average momentum and fluctuation energy equations for a homogeneous fluidized bed in the limit of high Stokes number and nearly elastic particles are given by

$$m \frac{dU}{dt} = mg - 6\pi\mu a R_{\text{drag}}(\phi) U, \quad (16)$$

$$\frac{3m}{2} \frac{dT}{dt} = \frac{a(6\pi\mu a)^2}{mT^{1/2}} U^2 S^*(\phi) - 18\pi\mu a T R_{\text{diss}}(\phi) - \frac{12m}{a\pi^{1/2}} (1-e)\phi\chi T^{3/2}. \quad (17)$$

The steady-state particle-phase temperature for elastic particles is given by

$$\frac{T}{U_t^2} = \left[\frac{S^*}{3StR_{\text{drag}}^2 R_{\text{diss}}} \right]^{2/3} \quad (18)$$

when $e = 1$ in agreement with our assumption that T/U^2 is small. In writing the above expression we have made use of the relation

$$\frac{U}{U_t} = \frac{1}{R_{\text{drag}}} \quad (19)$$

obtained from (16) at steady state and $mg = 6\pi\mu a U_t$. Substituting this estimate of T into the expression (final term on the right-hand side of (17)) for the energy dissipated by inelastic collisions, we find that the particles may be treated as elastic provided $1-e \ll St^{-2/3}$. If the dissipation by inelastic collisions is much larger than the viscous dissipation, then we obtain

$$\frac{T}{U_t^2} = \frac{\pi^{1/4}}{St} \left[\frac{S^*}{12(1-e)\phi\chi R_{\text{drag}}^2} \right]^{1/2} \quad (20)$$

which also vanishes as $St \rightarrow \infty$. In this case the expansion in the velocity field (7) proceeds in inverse powers of $St^{-1/2}$ but the resulting expression for the source remains the same. For fixed e we see that the non-dimensional particle temperature will undergo a transition from a $St^{-2/3}$ scaling at moderately large St to a St^{-1} scaling at very large St .

The drag coefficient R_{drag} in (18) is determined to leading order from the average of $F_{v,I}$. Since the average drag on a particle in a suspension where all the particles are moving with the same velocity U is the same as in the case of a fixed bed with an average velocity of the fluid $-U$, we note that R_{drag} to leading order is the same as the drag coefficient R_{fb} for fixed beds. Thus, for the case of elastic particles,

$$R_{\text{drag}} = R_{fb} + O(St^{-2/3}). \quad (21)$$

ϕ	N_s	$\text{var}(F_I)$	S	$S/\text{var}(F_I)$
0.35	2	2.3	0.46	0.20
	3	11.84	2.16	0.18
	4	11.85	2.29	0.19
	5	12.56	2.54	0.20
0.45	2	1.14	0.17	0.15
	3	22.79	3.68	0.16
	4	35.10	5.54	0.16
0.50	2	0.59	0.062	0.10
	3	27.10	2.91	0.11
	4	48.6	5.44	0.11

TABLE 1. S^* and $S^*/\text{var}(F_I)$ as functions of ϕ and N_s for random arrays with $N = 16$. The variance is non-dimensionalized by $(6\pi\mu aU)^2$. Note that, while both S^* and $\text{var}(F_I)$ vary significantly with N_s , their ratio is nearly constant.

The error of $O(St^{-2/3})$ in the above expression arises from the contribution to the total drag from \mathbf{v}_{III} .

2.2. Results for energy source S^* and mean drag R_{drag}

We have seen that to leading order the relative velocity \mathbf{v}_{II} of the particles is the same as that of a hard-sphere system. Thus, to determine $S^*(\phi)$ we carried out simulations in which the evolution of particle positions was determined by a molecular dynamics code. The leading-order viscous force $\mathbf{F}_{v,I}^\alpha$ is that associated with the gas motion produced by the mean velocity \mathbf{U} of all the particles. However, this force varies with time (non-dimensionalized by $a/T^{1/2}$) due to the changes in particle configuration obtained from a hard-sphere dynamics code with a non-dimensional temperature of unity. At time $t = 0$, \mathbf{v}_{III}^α is taken to be zero for all the particles. At subsequent times \mathbf{v}_{III} is determined by integrating (9) using Simpson's rule. At collision both \mathbf{v}_{III}^α and \mathbf{v}_{II}^α instantaneously change their values according to elastic collision rules. We found that the straightforward integration of (9) as mentioned above led to large fluctuations in $\langle \mathbf{v}_{III} \cdot \hat{\mathbf{F}}_{v,I} \rangle$. To reduce these statistical fluctuations, a small damping term $-6\pi\mu a\epsilon R_{\text{drag}} \mathbf{v}_{III}^\alpha$ was therefore added to the right-hand side of (9). The simulations were carried out typically with $\epsilon = 0.03$. Simulations for different values of ϵ in the range 0.01–0.05 were also carried out for selected values of ϕ , and the variations in ϵ were found to have no statistically significant effect on S^* .

The forces on the particles were evaluated using the method described in Mo & Sangani (1994) in which N particles are placed in a unit cell periodically repeated in space and the velocity disturbance due to each particle is expressed in terms of a series of multipoles. Table 1 shows results of simulations for three different values of volume fraction ϕ . N_s indicates the largest order of the multipoles retained in the expansion. The total number of multipoles is then $(3N_s^2 - 1)N$. We see that even though both S^* and the variance of the viscous force, $F_{v,I}$, change considerably with N_s , the ratio of the two is approximately constant for a given ϕ . If we interpret S^* as a product of the force variance and a correlation time, then the results of table 1 suggest that the correlation time is essentially independent of N_s . Calculation of S^* requires averaging over several thousand time steps in order to determine the correlation time with reasonable accuracy and the simulations with high N_s are, as a consequence, computationally very intensive. We can, however, take advantage of the

ϕ	N	N_s	$\langle F_I \rangle$	$\text{var}(F_I)$	$\text{var}(F_I)/\langle F_I \rangle^2$
0.01	128	1	1.28	0.079	0.048
0.03	128	1	1.50	0.230	0.102
0.05	54	2	1.91	0.285	0.078
		2	1.88	0.287	0.081
0.07	128	1	2.15	0.455	0.098
0.15	32	2	3.6	1.01	0.078
		3	3.84	1.21	0.082
		4	3.87	1.25	0.083
0.35	32	3	12.74	12.16	0.075
		4	13.60	14.89	0.081
		5	13.91	14.57	0.086
		6	14.1	17.25	0.086
0.45	32	3	22.86	30.4	0.058
		4	25.63	44.8	0.068
		5	27.02	52.7	0.072
		6	27.51	61.0	0.081
0.50	32	3	31.32	55.63	0.057
		4	36.38	89.72	0.068
		5	39.45	115.7	0.074
		6	41.10	135.7	0.080

TABLE 2. $\text{var}(F_I)/\langle F_I \rangle^2$ as a function of N_s . The results are obtained by averaging over 30 independent hard-sphere configurations. Note that the ratio is approximately constant and equal to 0.08 for $\phi \geq 0.15$. The average force and variance are non-dimensionalized by, respectively, $6\pi\mu aU$ and $(6\pi\mu aU)^2$.

fact that the correlation time is relatively insensitive to N_s and determine its value from simulations with lower values of N_s . The force variance must be computed using higher N_s , but its value can be determined from a relatively small number of independent hard-sphere configurations.

Table 2 gives results for the force variance as a function of ϕ and N_s , which were obtained by averaging over thirty independent hard-sphere configurations. Both the average drag force $\langle F_{v,I} \rangle$ and the variance are sensitive to the volume fraction but the ratio of variance to average drag force squared is nearly constant at about 0.085 for ϕ greater than about 0.15.

The analysis of Koch (1990) for dilute suspensions gave $S^* = 1/(2\pi^{1/2})$. Therefore we present the results for S^* in figure 1 in terms of R_s defined by

$$S^* = \frac{1}{2\pi^{1/2}} R_s R_{\text{drag}}^2. \quad (22)$$

R_s represents the energy source due to a specified mean force acting on the particles whereas S^* is the source for a specified mean relative velocity of the particles and gas. Note that $R_s \rightarrow 1$ as $\phi \rightarrow 0$. For $\phi \geq 0.45$ we determined the fixed-bed drag coefficient R_{drag} using $N = 16$ and $N_s = 6$ while the correlation time was estimated using $N_s = 3$ or 4 and $N = 64$. We found the correlation time at such high volume fractions to be approximately proportional to the average collision time for the hard-sphere systems. For example, the ratio of collision times at $\phi = 0.53$ for simulations with $N = 16$ and $N = 64$ was 1.28 and the ratio of correlation times for the same values of N was about 1.25. The spatial configurations of hard-sphere systems change significantly at

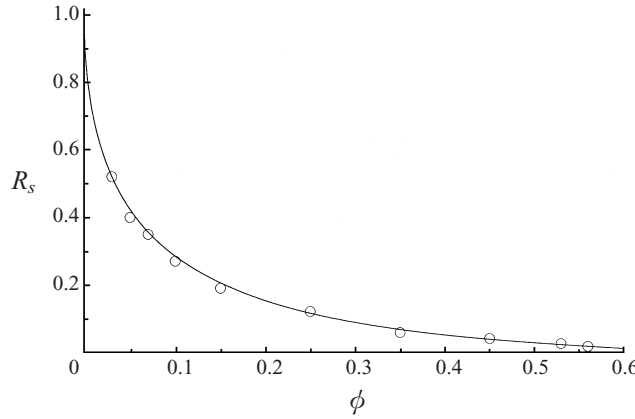


FIGURE 1. R_s as a function of ϕ . The circles represent the simulation results and the line represents (23).

such high volume fractions with N , and this makes it necessary to use larger values of N at high volume fractions. On the other hand, Koch's analysis suggests that at very low volume fractions the correlation time is proportional to the time it takes for a pair of particles to separate from each other by the Brinkman length of $O(a/\phi^{1/2})$. This requires that the unit cell be large compared with the Brinkman length, or that N be large enough. The results for $\phi = 0.03$ and 0.05 were therefore obtained with, respectively, $N = 256$ and $N = 128$. The number of multipoles $((3N_s^2 - 1)N)$ required in determining the forces on the particles is large for these situations, and we used the $O(N)$ algorithm described in Sangani & Mo (1996) to enhance the efficiency of the computations for $\phi \leq 0.05$ and $\phi \geq 0.45$.

As shown in figure 1 the numerical results for R_s can be represented well by the expression

$$R_s = \frac{1}{\chi(1 + 3.5\phi^{1/2} + 5.9\phi)}, \quad (23)$$

where χ is the value at contact, $r = 2a$, of the radial distribution function for a hard-sphere system which is given by Ma & Ahmadi (1988) as

$$\chi = \frac{1 + 2.5\phi + 4.5094\phi^2 + 4.515439\phi^3}{[1 - (\phi/0.64356)^3]^{0.678021}}. \quad (24)$$

The rationale for fitting the numerical results according to (23) is as follows. At high volume fraction, the correlation time appears to be proportional to the average collision time, which, in turn, is expected to be inversely proportional to χ . The above expression for χ by Ma & Ahmadi suggests that this correlation time will vanish at $\phi = 0.64356$ which is the maximum packing density for spheres in a random array. The first variation of R_s from 1 at low volume fractions is expected to be $O(\phi^{1/2})$ because of the dependence of the correlation time on Brinkman screening length.

Results for the fixed-bed drag coefficient R_{drag} were obtained previously using a multipole method by Ladd (1990) for $\phi \leq 0.45$. Our results are in very good agreement with his as shown in table 3. For higher volume fractions, the empirical correlation by Carman (1937)

$$R_c = \frac{10\phi}{(1 - \phi)^3} \quad (25)$$

ϕ	N_s	R_{drag}	Ladd	Eq. (26)	Carman
0.05	2	1.90	1.89	1.99	—
0.15	4	3.88	3.85	4.04	—
0.25	5	7.3	7.3	7.3	—
0.35	5	14.1	14.1	13.6	—
0.45	5	28	28.2	28.2	27.75
0.50	7	41	—	—	40.7
0.53	6	52	—	—	51.8
0.56	6	64	—	—	66.4
0.61	9	105	—	—	103.5

TABLE 3. R_{drag} as a function of ϕ . The result for $\phi = 0.61$ is taken from Mo & Sangani (1994). Shown also are the corresponding results obtained by Ladd (1990), equation (26), and the Carman correlation, (23).

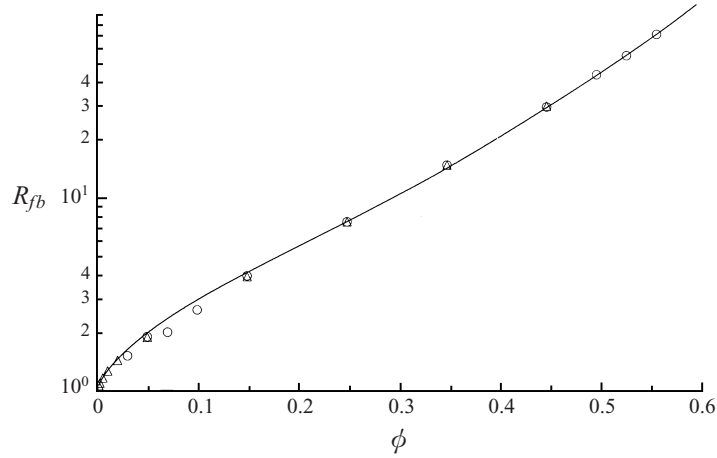


FIGURE 2. R_{fb} as a function of ϕ . The circles are our simulation results, the triangles are the simulations of Ladd (1990) and the line represents the expressions (26) for $\phi < 0.4$ and (25) (with 0.7 added to its right-hand side) for $\phi > 0.4$.

is known to provide reasonably accurate estimates. Our results for $\phi > 0.4$ are indeed in good agreement with Carman's expression.

For the stability analysis it will be necessary to have an analytical fit for the numerical results for R_{drag} as well. We shall use

$$R_{\text{drag}} = \frac{1 + 3(\phi/2)^{1/2} + (135/64)\phi \ln \phi + 17.14\phi}{1 + 0.681\phi - 8.48\phi^2 + 8.16\phi^3} \quad (\phi < 0.4). \quad (26)$$

The above expression agrees to $O(\phi)$ with the theoretical expression for the drag in dilute fixed beds (Howells 1974; Hinch 1977; Kim & Russel 1985) and with the results of numerical simulations as can be seen from figure 2. For $\phi \geq 0.4$ we shall use the much simpler expression given by Carman (25) with a small addition of 0.7 to its right-hand side which renders the values of R_{drag} given by the two expressions equal at $\phi = 0.4$. Figure 2 shows a comparison between the numerical results and the above expressions for R_{drag} .

Finally, we shall also need $R_{\text{diss}}(\phi)$ to compute the particle velocity variance. The viscous energy dissipation in a suspension with a Maxwellian particle velocity

distribution was evaluated by Sangani *et al.* (1996) who obtained

$$R_{\text{diss}} = 1 + 3(\phi/2)^{1/2} + (135/64)\phi \ln \phi + 11.26\phi \times (1 - 5.1\phi + 16.57\phi^2 - 21.77\phi^3) - \phi\chi \ln \epsilon_m. \quad (27)$$

The above expression agrees that for R_{drag} up to terms of $O(\phi \ln \phi)$. At $O(\phi)$ the two expressions differ since the $O(\phi)$ coefficient depends on the details of pair interactions and the velocities of the particles are different in the two problems. R_{diss} is determined for Maxwell-distributed particle velocities with zero mean and R_{drag} for particles with a common velocity relative to the gas. The energy dissipated in the gap between two particles having a non-zero relative velocity and separated by a gap width of ϵ increases as $1/\epsilon$ as $\epsilon \rightarrow 0$ if one assumes that the standard incompressible, continuum lubrication flow between smooth, rigid, spherical particles is applicable at all particle separations. The resulting R_{diss} would be infinite. Sangani *et al.* (1996) allowed for the breakdown of the usual lubrication analysis for the particles with the gap width less than $2\epsilon_m a$. The resulting R_{diss} therefore diverges logarithmically with ϵ_m . For gas–solid suspensions the most likely cause of the lubrication breakdown is non-continuum effects in the gas since the mean free path λ of the gas molecules is typically about 1000 Å. Sundararajakumar & Koch (1996) have determined the energy dissipation in the gap between colliding particles accounting for the finite mean free path of the molecules and their analysis indicates that using

$$\epsilon_m = 4.88(\lambda/a) \quad (28)$$

in expression (27) for R_{diss} will yield the correct rate of dissipation. Gopinath, Chen & Koch (1997) have shown that ϵ_m may also depend on the compressibility of the gas for larger particles and larger velocity differences between the particles. However, the qualitative behaviour of the suspension will not be very sensitive to the exact nature of lubrication breakdown since it only contributes a weak logarithmic factor.

3. Moderate-Stokes-number suspensions of slightly inelastic particles

In the preceding development, we have assumed that the velocity distribution function is controlled by the elastic collisions among the particles and is therefore an isotropic Maxwellian. This requires that the mean-free time between collisions be much smaller than the viscous relaxation time. In a dilute suspension, this occurs for very massive particles with $St \gg \phi^{-3/2}$. In the regime $\phi^{-3/4} \ll St \ll \phi^{-3/2}$, corresponding to moderately massive particles, the particle velocities do not relax to the local fluid velocity but the velocity distribution function is controlled by hydrodynamic interactions rather than collisions. Hydrodynamic interactions feed more energy into the vertical particle velocity fluctuations than the horizontal. As a consequence, the anisotropy in velocity fluctuations is quite significant in moderate-to-low-Stokes-number suspensions. As in the case of Sangani *et al.* (1996) and Kang *et al.* (1997) we shall develop an approximate kinetic theory for the moderate-Stokes-number case using a Grad approximation for evaluating the collisional terms in the balance equation. The hydrodynamic source of particle fluctuating energy will be approximated as the anisotropic tensor derived by Koch (1990) modulated by a function of particle volume fraction computed from the high-Stokes-number simulations presented in the previous section.

To determine the anisotropy in the velocity variance we need balance equations for the second moments of the fluctuating velocity $C_i^\alpha = v_i^\alpha - \langle v_i \rangle$. An equation for the

second moment $T_{ij} \equiv \langle C_i^\alpha C_j^\alpha \rangle$ can be readily obtained from (1) and (2) and is given by

$$m \frac{dT_{ij}}{dt} = \langle C_i^\alpha (F_{j,v}^\alpha - \langle F_{j,v} \rangle) \rangle + \langle C_j^\alpha (F_{i,v}^\alpha - \langle F_{i,v} \rangle) \rangle + \langle C_i^\alpha F_{j,c}^\alpha + C_j^\alpha F_{i,c}^\alpha \rangle. \quad (29)$$

Now we decompose the right-hand side into the source and sink tensors resulting from various mechanisms. For example, the sink due to viscous dissipation is expressed as

$$\Gamma_{ij,v} = -6\pi\mu a R_{\text{diss}}(\phi) T_{ij}. \quad (30)$$

Sangani *et al.* (1996) used the above sink term in their kinetic theory for sheared gas–solid suspensions and found that the even though R_{diss} was determined for high-Stokes-number suspensions with isotropic Maxwellian distributions, the resulting theory predicted the velocity moments reasonably accurately even when Stokes number was not large. The source due to hydrodynamic interactions will be expressed as

$$S_{ij,h} = \frac{a(6\pi\mu a)^2}{mT^{1/2}} [(S_{\parallel}^* - S_{\perp}^*) U_i U_j + S_{\perp}^* U^2 \delta_{ij}]. \quad (31)$$

Koch (1990) derived the vertical (S_{\parallel}^*) and horizontal (S_{\perp}^*) components of the source tensor in the above expression for dilute sedimenting suspensions. We shall assume that the same expressions hold for non-dilute suspensions when his expressions are multiplied by the factor $R_s(\phi)R_{\text{drag}}^2(\phi)$ that accounts for higher-order particle interactions in high-Stokes-number suspensions, i.e. we assume

$$S_{\parallel}^* = \frac{3}{16\pi^{1/2}} \left(\frac{T}{T_{\parallel}} \right)^{1/2} R_s R_{\text{drag}}^2 \left[(\beta^5 + \beta) \ln \left(\frac{\beta + 1}{\beta - 1} \right) - \frac{2}{3}\beta^2 - 2\beta^4 \right], \quad (32)$$

$$S_{\perp}^* = \frac{3}{16\pi^{1/2}} \left(\frac{T}{T_{\parallel}} \right)^{1/2} R_s R_{\text{drag}}^2 \left[\frac{1}{2}(\beta^3 - \beta^5) \ln \left(\frac{\beta + 1}{\beta - 1} \right) - \frac{2}{3}\beta^2 + \beta^4 \right], \quad (33)$$

where $\beta^2 = T_{\parallel}/(T_{\parallel} - T_{\perp})$ and T_{\parallel} and T_{\perp} are, respectively, the variance in the velocity components parallel and perpendicular to \mathbf{U} .

The collisional change of the second moment of velocity in (29) can be evaluated using a Grad approximation as was done by Jenkins & Richman (1985) and Sangani *et al.* (1996). Setting the velocity gradient terms in (4.21) of Sangani *et al.* (1996) to zero we obtain

$$S_{ij,c} - \Gamma_{ij,c} = \frac{24m}{5a\pi^{1/2}} \phi \chi (1 + e) T^{1/2} \left[\frac{1}{3}(2 + e) T \delta_{ij} - \left(\frac{3}{2} - \frac{1}{2}e \right) T_{ij} \right]. \quad (34)$$

The trace of the above expression for nearly elastic particles ($0 < 1 - e \ll 1$) is the same as the expression (6) for $-\Gamma_{\text{inelas}}$ given earlier. The terms inside the square brackets in (34) reduce to $T \delta_{ij} - T_{ij}$ when the coefficient of restitution is unity indicating the tendency of the collisions to drive the velocity distribution towards an isotropic Maxwellian.

Collecting all the terms, the balance equation for the second moments becomes

$$\begin{aligned} \frac{a}{U_t} \frac{dT_{ij}}{dt} = & -\frac{R_{\text{diss}}}{St} T_{ij} + \frac{U_t}{T^{1/2}} \frac{1}{St^2} \{ S_{\perp}^* U^2 \delta_{ij} + (S_{\parallel}^* - S_{\perp}^*) U_i U_j \} \\ & + \frac{24}{5\pi^{1/2}} \phi \chi (1 + e) \frac{T^{1/2}}{U_t} \left[\frac{1}{3}(2 + e) T \delta_{ij} - \left(\frac{3}{2} - \frac{1}{2}e \right) T_{ij} \right]. \end{aligned} \quad (35)$$

In the limit of large St and small $1 - e$ the collision term forces the velocity distribution to become isotropic ($\beta \rightarrow \infty$), and the trace of the above equation reduces to (17)

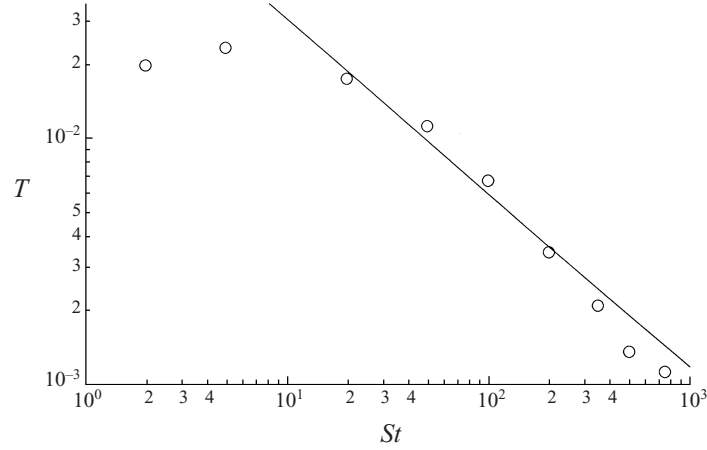


FIGURE 3. The velocity variance as a function of Stokes number for a suspension of perfectly elastic particles with $\phi = 0.02$ and $N = 16$. The circles are the results of dynamic simulations and the line is the theoretical result given by (18).

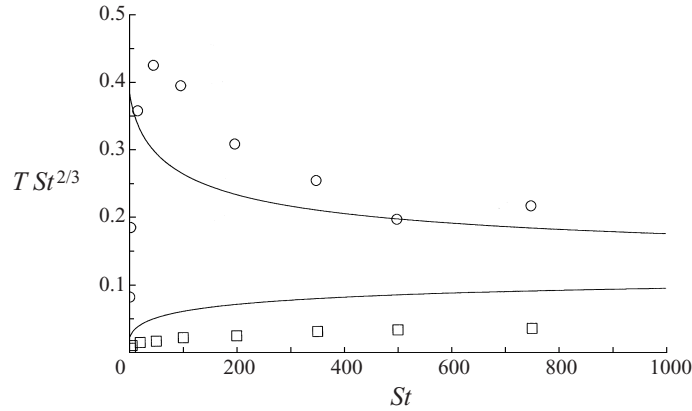


FIGURE 4. The scaled vertical and horizontal components of the second moment of the particle velocity are plotted as a function of Stokes number for perfectly elastic particles. The circles and upper curve represent the dynamic simulations and the theoretical result obtained from (35), respectively, for $T_{\parallel} St^{2/3}$. The squares and lower curve are the dynamic simulation and theoretical results for $T_{\perp} St^{2/3}$.

derived in the previous section. For dilute suspensions with $e = 1$ and $\phi^{-3/4} \ll St \ll \phi^{-3/2}$ the collision term in the above equation is negligible as shown by Koch (1990). His analysis gave

$$\frac{T_{\parallel}}{U_t^2} = 0.802 St^{-2/3}, \quad \frac{T_{\perp}}{U_t^2} = 0.034 St^{-2/3}. \quad (36)$$

Note that the anisotropy of the variance is very large in this limit. The variance can be estimated for arbitrary ϕ and St by keeping all the terms in (35) and solving the resulting equations numerically.

The theoretical results for $\phi = 0.02$ and $e = 1$ are shown in figures 3 and 4 where they are compared with the results obtained by the direct numerical simulations to be described in § 5. At low Stokes number, the simulated velocity variance reaches a constant value characteristic of an inertialess suspension, cf. figure 3. As the Stokes

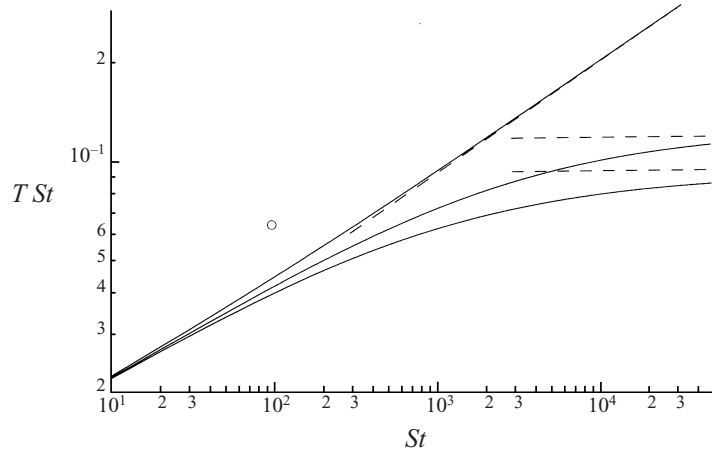


FIGURE 5. The scaled velocity variance $T St$ is plotted as a function of Stokes number for suspensions of particles with coefficients of restitution $e = 1, 0.9$, and 0.8 and $\phi = 0.05$. The solid curves are the theoretical results. The dashed lines correspond to the large-Stokes-number asymptotes (18) and (20). The circle is the result of dynamic simulations for $e = 1$, $N = 16$, and $St = 50$.

number is increased the Brinkman screening of the hydrodynamic interactions among the particles leads to a velocity variance that decreases in proportion to $St^{-2/3}$. In view of this high-Stokes-number scaling, we plot the products $T_{\parallel} St^{2/3}$ and $T_{\perp} St^{2/3}$ as a function of the Stokes number in figure 4. At low Stokes numbers, the collisions have relatively little effect on the velocity variance and the anisotropy of the hydrodynamic-interaction source leads to a large ratio of T_{\parallel}/T_{\perp} . As St increases, collisions become increasingly rapid compared with viscous relaxation and the velocity distribution becomes increasingly isotropic. Figure 5 illustrates the effects of inelastic interparticle collisions on the velocity variance. Results are presented for $\phi = 0.05$ with coefficients of restitution $e = 0.8, 0.9$ and 1 . The dashed lines indicate the high-Stokes-number asymptotes (18) and (20). It can be seen that the variance for perfectly elastic particles scales like $St^{-2/3}$ over the full range of Stokes numbers, $St > 10$ shown. On the other hand, the inelastic particles exhibit a transition from a $St^{-2/3}$ scaling at moderate St to a St^{-1} scaling at very high Stokes numbers. The circle indicates the velocity variance obtained in a dynamic simulation with 16 particles in a unit cell. The variance is approximately 40% higher than the theory. The additional variance observed in the dynamic simulation can be attributed to the inhomogeneous structure that develops in this unstable suspension. This will be discussed further in the forthcoming sections.

4. Stability analysis

In this section, we will introduce equations of motion applicable to an inhomogeneous fluidized bed and perform a linear stability analysis to determine the conditions under which a homogeneous bed is unstable to waves of particle concentration. Previous studies (Didwania & Homsy 1982; Anderson *et al.* 1995; Glasser *et al.* 1997; Goz 1995; Harris & Crighton 1994; Batchelor 1988, 1993) of fluidized bed stability have indicated that waves with the wave vector parallel to gravity (vertical waves) have the largest growth rate. Thus, the initial instability involves vertical waves, although horizontal structure may set in subsequently. We will restrict ourselves to determining the form of the initial instability and will therefore consider only vertical

waves in which the average particle velocity $\langle \mathbf{U} \rangle = \mathbf{e}_3 U$ is in the vertical direction and the dependent variables U , ϕ , T , and T_{\parallel} are functions of the vertical coordinate $z = \mathbf{e}_3 \cdot \mathbf{x}$ and time t only. The average mixture velocity $\langle \mathbf{u} \rangle$ will be taken to be zero.

The traditional particle-phase equations of motion for fluidized beds have included mass and momentum conservation equations. The momentum conservation equation included a particle pressure which was assumed to be a function of the volume fraction only. In our treatment based on the kinetic theory of granular materials, one finds that the particle pressure is related to a particle-phase temperature as well as the volume fraction. Thus, we require additional conservation equations for the kinetic energy associated with the particle velocity fluctuations. We found in §3 that the anisotropy of the velocity variance is often quite significant and so we will consider separate conservation equations for the vertical velocity variance T_{\parallel} and the overall variance $3T = T_{\parallel} + 2T_{\perp}$.

Non-dimensionalizing U and $T^{1/2}$ by the terminal velocity U_t , z with the particle radius a , and t by a/U_t , the equations of mass and momentum conservation reduce to

$$\frac{\partial \phi}{\partial t} + \frac{\partial}{\partial z}(\phi U) = 0, \quad (37)$$

$$\phi \left[\frac{\partial U}{\partial t} + U \frac{\partial U}{\partial z} \right] = \frac{\phi}{St} - \frac{\phi R_{\text{drag}}}{St} U - \frac{\partial P_m}{\partial z} + \frac{\partial}{\partial z} \left[\mu_c \frac{\partial U}{\partial z} \right]. \quad (38)$$

The above equations are the same as those given in our treatment of a sheared gas–solid suspension (cf. (4.13)–(4.16) and (4.22) from Sangani *et al.* 1996) except that the momentum equation contains a body force, ϕ/St , due to gravity. In (38)

$$P_m = (\phi + 8B/5)T_{\parallel} + (12/5)BT, \quad (39)$$

$$\mu_c = \frac{48}{5\pi^{1/2}} B T^{1/2}, \quad (40)$$

$$B = \phi^2 \chi \eta, \quad \eta = (1 + e)/2. \quad (41)$$

The left-hand side of (38) contains the particle-phase inertia terms. The second term on the right-hand side is the mean drag per unit volume exerted by the gas on the particles; this force is a function of volume fraction owing to the hydrodynamic interactions among the particles and the dependence of R_{drag} on ϕ plays a crucial role in the instability. The third term is the divergence of a stress P_m given by (39). This stress contains terms proportional to the particle velocity variances T and T_{\parallel} . These variances are different from those obtained for a homogeneous suspension in the previous section and contain contributions proportional to $\partial U / \partial z$ (see (42) and (43) below). Thus, the third term on the right-hand side of (38) includes both pressure gradient and viscous stress terms. The fourth term on the right-hand side of (38) is an additional viscous stress contribution due to the collisional stress.

The solution of (39) and (35) for the vertical particle pressure in a homogeneous fluidized bed indicates that P_m scales like $St^{-2/3}$ in the limit of large Stokes number. The pressure is non-dimensionalized with $\rho_p U_t^2$ where ρ_p is the mass density of a particle. Since U_t is proportional to a^2 and $St \sim a^3$, the dimensional pressure is predicted to be proportional to the particle radius squared. This scaling of the particle pressure with particle radius (at a constant ratio of the superficial to the minimum fluidization velocity) has been observed in experimental studies by Cody *et al.* (1996) in non-bubbling gas fluidized beds. On the other hand, Campbell & Wang (1991) showed that the particle pressure in a bubbling gas-fluidized bed was well correlated

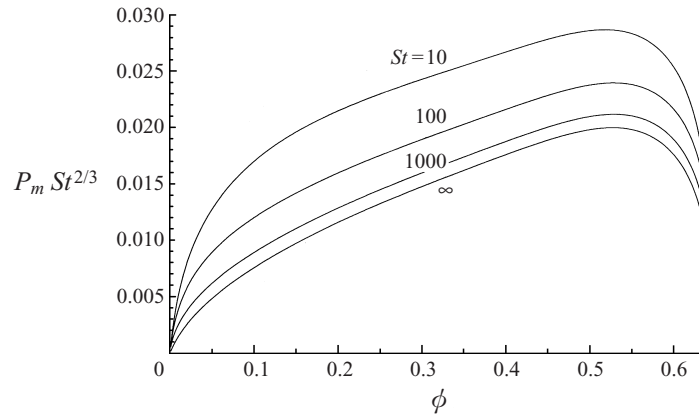


FIGURE 6. The scaled vertical particle pressure $P_m St^{2/3}$ is plotted as a function of the volume fraction for a suspension of perfectly elastic particles with $St = 10, 100, 1000$, and ∞ .

with the bubble-diameter suggesting that the pressure is produced primarily by the bubble-induced flow in this inhomogeneous situation.

Figure 6 illustrates the variation of $P_m St^{2/3}$ with volume fraction for $St = 10, 100, 1000$, and ∞ . In the dilute limit, the source and dissipation of energy approach constant values. Thus, the granular temperature is finite as $\phi \rightarrow 0$ and the pressure is proportional to ϕ . As the particle concentration increases, two competing factors influence the particle pressure. For a given particle temperature, the particles in a dense bed undergo more frequent collisions. However, the source of energy decreases and the viscous dissipation of energy increases with increasing volume fraction. The net result is that the particle pressure passes through a maximum at $\phi \approx 0.5$ and then diminishes as one approaches the close-packed limit. Zenit, Hunt & Brennen (1997) have observed a similar qualitative variation of the particle pressure with volume fraction in liquid-fluidized beds at large Stokes and Reynolds numbers. However, the absolute magnitude of the particle pressure was considerably larger than that predicted here for a *homogeneous, low-Reynolds-number, gas-fluidized bed*. The scaled vertical pressure $P_m St^{2/3}$ is high at moderate Stokes numbers owing to the anisotropy of the source of particle fluctuation energy and eventually reaches a finite high-Stokes-number asymptote corresponding to a state where interparticle collisions efficiently exchange energy between the vertical and horizontal particle motions.

Figure 7 illustrates the effects of inelastic interparticle collisions on the granular pressure. The vertical pressure P_m is plotted as a function of particle volume fraction for $St = 100$ and three coefficients of restitution $e = 0.8, 0.9$, and 1 . The inelastic collisions lead to a modest decrease in the granular pressure that is most significant at intermediate volume fractions.

In the dilute limit, particle collisions are infrequent compared with interparticle hydrodynamic interactions (which occur at interparticle separations comparable with the Brinkman screening length), so the dissipation due to inelastic collisions is unimportant. At high volume fractions, the granular temperature becomes quite small. Since the viscous dissipation is proportional to T while the loss due to inelastic collision scales like $T^{3/2}$, the small granular temperature makes viscous dissipation more important than the energy lost due to solid-body collisions.

Equations for the second moments of the velocity distribution in an inhomogeneous suspension can be obtained using (4.8), (4.10), (4.21), and (4.22) of Sangani *et al.*

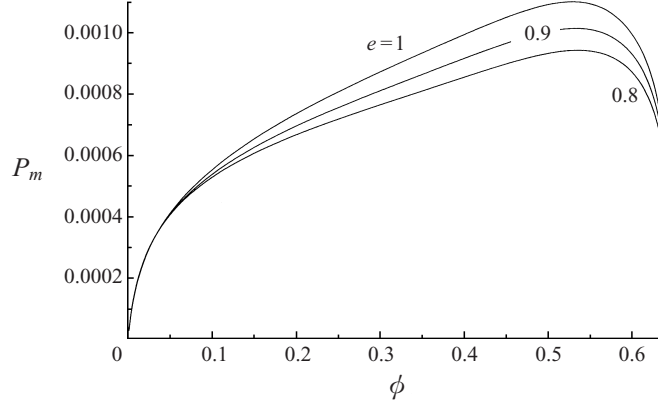


FIGURE 7. The vertical particle pressure is plotted as a function of particle volume fraction for $St = 100$ and three values of the coefficient of restitution $e = 1, 0.9$, and 0.8 .

(1996). Thus, the conservation equations for the vertical velocity variance T_{\parallel} and the overall variance $3T$ are

$$\frac{1}{2}\phi \left[\frac{\partial T_{\parallel}}{\partial t} + U \frac{\partial T_{\parallel}}{\partial z} \right] = \frac{1}{3} \frac{\partial}{\partial z} \left(\kappa \frac{\partial T_{\parallel}}{\partial z} \right) - P_m \frac{\partial U}{\partial z} + \mu_c \left(\frac{\partial U}{\partial z} \right)^2 + S_{\parallel} - \Gamma_{\parallel}, \quad (42)$$

$$\frac{3}{2}\phi \left[\frac{\partial T}{\partial t} + U \frac{\partial T}{\partial z} \right] = \frac{\partial}{\partial z} \left(\kappa \frac{\partial T}{\partial z} \right) - P_T \frac{\partial U}{\partial z} + \mu_c \left(\frac{\partial U}{\partial z} \right)^2 + S - \Gamma. \quad (43)$$

Sangani *et al.* only presented results for a spatially homogeneous suspension. When we generalize their equation (4.20) to inhomogeneous time-dependent suspensions, we encounter terms involving third moments $\langle C_3^3 \rangle$ and $\langle C_3 C^2 \rangle$ associated with the fluxes of vertical and overall temperatures. To obtain closed equations of motion, we have assumed that the fluxes of vertical and total energy can be written as $-(\frac{1}{3})\kappa(\partial T_{\parallel}/\partial z)$ and $-\kappa(\partial T/\partial z)$, where

$$\kappa = \frac{8}{\pi^{1/2}} \phi^2 \chi T_{\parallel}^{1/2} \left(1 + \frac{25\pi}{512\phi^2 \chi^2} \right) \quad (44)$$

is the thermal conductivity for an isotropic gas with temperature T_{\parallel} . We use the vertical temperature in (44) since we are interested in the vertical flux of energy.

The left-hand sides of (42) and (43) represent the convection of vertical and overall fluctuation energy, respectively. The first terms on the right-hand sides are the divergences of the thermal fluxes. The second and third terms are the work done by the stress, i.e. pressure work and viscous dissipation, where

$$P_T = 4BT(3\eta - 2). \quad (45)$$

The last two terms on the right-hand sides of (42) and (43) are the sources and dissipations of vertical and overall energy:

$$S_{\parallel} - \Gamma_{\parallel} = \frac{S_{\parallel}^* U^2 \phi}{St^2 T^{1/2}} - \frac{\phi R_{\text{diss}} T_{\parallel}}{St} - \frac{24}{5\pi^{1/2}} B T^{1/2} [(2 - \eta)T_{\parallel} - \frac{1}{3}(1 + 2\eta)T], \quad (46)$$

$$S - \Gamma = \frac{S^* U^2 \phi}{St^2 T^{1/2}} - \frac{3\phi R_{\text{diss}} T}{St} - \frac{24}{\pi^{1/2}} (1 - \eta) B T^{3/2}, \quad (47)$$

with $S^* = S_{\parallel}^* + 2S_{\perp}^*$.

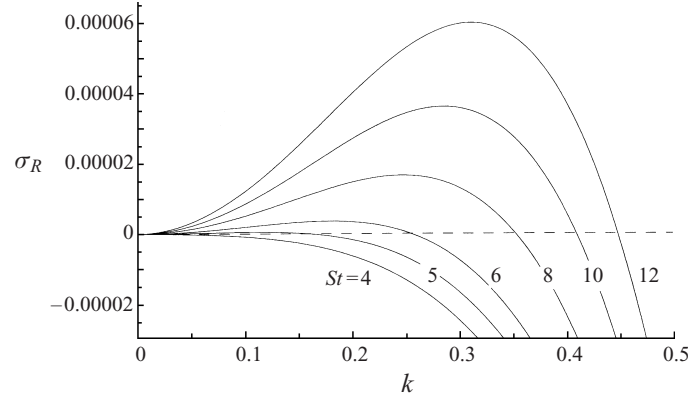


FIGURE 8. The growth rate of vertical volume fraction waves is plotted as a function of the wavenumber for $\phi = 0.5$, $e = 1$, and $St = 4, 5, 6, 8, 10$, and 12 .

The effect of hydrodynamic interaction forces was purely dissipative in Sangani *et al.*'s analysis of sheared gas–solid suspensions in the absence of gravity and it led to the second terms on the right-hand sides of (46) and (47). However, the fluctuating force associated with the gas-velocity disturbance induced by the particles' gravitational settling creates sources of energy represented by the first term. The third term on the right-hand side of (47) is the dissipation of total energy due to inelastic collisions, whereas the corresponding term in (46) involves a collisional exchange of energy between vertical and horizontal fluctuations as well as an inelastic dissipation.

In the absence of spatial and temporal gradients of average properties, the equations of motion have a unique solution for velocity, temperature and T_{\parallel}/T given by (18), (19), and the implicit result obtained by setting the right-hand side of (35) to zero. To assess the stability of the homogeneous state, we substitute a solution of the form

$$\Psi = \Psi_0 + \epsilon \hat{\Psi} \exp(ikz + \sigma t) \quad (48)$$

into the equations of motion (37), (38), (42), and (43). Here, Ψ represents the dependent variables ϕ , U , T , and T_{\parallel} , σ is the growth rate, k is the wavenumber, Ψ_0 is the base state, and ϵ is the amplitude of the perturbation. Linearizing the resulting equations for $\epsilon \ll 1$, we can solve for the relative amplitudes U/ϕ , T/ϕ , and T_{\parallel}/ϕ and obtain a fourth-order polynomial dispersion equation for the growth rate $\sigma(k)$. This dispersion equation is rather long and will not be presented here. We find that three of the solutions for σ remain negative for all values of k . The fourth root, which controls the stability starts from the origin, i.e. $\sigma = 0$ at $k = 0$.

The real part of this root is plotted as a function of k for perfectly elastic particles with a volume fraction of 0.5 and several values of the Stokes number in figure 8. Below a critical Stokes number of $St_c = 4.36$, the growth rate is always negative indicating that perturbations of all wavelengths decay and the suspension is stable. At higher St , the growth rate first increases taking on positive values, then passes through a maximum, and eventually becomes negative. At the larger wavenumbers, the perturbations are damped primarily by the particle-phase viscosity and conductivity. Thus, above the critical Stokes number St_c , an unbounded suspension is unstable and the instability involves perturbations with wavenumbers between 0 and some maximum unstable wavenumber k_m .

At small volume fractions a slightly different behaviour is observed as illustrated

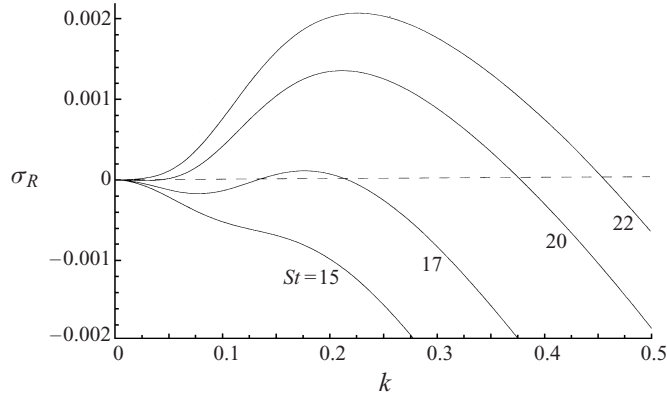


FIGURE 9. The growth rate of vertical volume fraction waves is plotted as a function of the wavenumber for $\phi = 0.02$, $e = 1$, and $St = 15, 17, 20$, and 22 .

in figure 9 for perfectly elastic particles with a volume fraction of 0.02. In this case, the growth rate is negative for all wavenumbers for $St < 16$. For a small range of intermediate Stokes numbers $17 < St < 21.2$, the growth rate starts from zero at $k = 0$, becomes negative, passes through a minimum, becomes positive and finally passes through a maximum and becomes negative again. At $St > 21.2$, the behaviour of $\sigma(k)$ is similar to that observed above the critical Stokes number in the dense suspension $\phi = 0.5$ discussed above.

A simple criterion for the marginal stability of an unbounded suspension can be obtained by considering the small-wavenumber behaviour of $\sigma(k)$. Near $k = 0$, the growth rate can be expanded in a Taylor series of the form:

$$\sigma = ik\sigma_1 + k^2\sigma_2 + O(k^3), \quad (49)$$

where σ_1 and σ_2 are purely real. The first term $ik\sigma_1$ represents a propagation of the wave with wave speed σ_1 and the stability of the suspension in the long-wavelength limit is determined by the sign of σ_2 . A positive value of σ_2 provides a sufficient but not a necessary condition for instability of the unbounded suspension. For dense suspensions, the Stokes number at which σ_2 becomes positive corresponds exactly to the marginal stability limit. In dilute suspensions, there is a narrow range of Stokes numbers for which $\sigma_2 < 0$ but the growth rate becomes positive at higher wavenumbers. Nonetheless, we will adopt the condition $\sigma_2 = 0$ as an approximate criterion for the marginal stability of the homogeneous suspension. In the case $\phi = 0.02$, this leads to an estimate $St_c = 21.2$ whereas the actual critical Stokes number is between 16 and 17.

Thus, the critical Stokes number will be estimated by substituting (49) into the full dispersion relation and setting terms of $O(k)$ and $O(k^2)$ to zero. This procedure indicates that the thermal convection and conduction terms have no effect on σ_1 and σ_2 and the energy equations reduce to the simple algebraic equations:

$$S_{\parallel} = \Gamma_{\parallel}, \quad S = \Gamma. \quad (50)$$

In other words, the time for thermal convection or conduction over large wavelengths is sufficiently long that a local balance of sources and sinks of energy controls the particle-phase temperatures. The linearized momentum and mass conservation

equations take the form

$$\alpha \hat{\phi} + ik\phi_0 \hat{U} = 0, \quad (51)$$

$$\left[\alpha \phi_0 + \mu_c k^2 + ik \left(\frac{\partial P_m}{\partial U} \right)_\phi + \frac{\phi_0 R_{\text{drag}}}{St} \right] \hat{U} + \left[ik \left(\frac{\partial P_m}{\partial \phi} \right)_U + \frac{R'_{\text{drag}} \phi_0}{St R_{\text{drag}}} \right] \hat{\phi} = 0, \quad (52)$$

where $\alpha = \sigma + ikU_0$ and the partial derivatives of pressure in (52) can be evaluated using

$$\left(\frac{\partial P_m}{\partial \phi} \right)_U = \left(\frac{\partial P_m}{\partial \phi} \right)_{U,T,T_\parallel} + \left(\frac{\partial P_m}{\partial T} \right)_{\phi,U,T_\parallel} \left(\frac{\partial T}{\partial \phi} \right)_U + \left(\frac{\partial P_m}{\partial T_\parallel} \right)_{\phi,U,T} \left(\frac{\partial T_\parallel}{\partial \phi} \right)_U, \quad (53)$$

$$\left(\frac{\partial P_m}{\partial U} \right)_\phi = \left(\frac{\partial P_m}{\partial T} \right)_{\phi,U,T_\parallel} \left(\frac{\partial T}{\partial U} \right)_\phi + \left(\frac{\partial P_m}{\partial T_\parallel} \right)_{\phi,U,T} \left(\frac{\partial T_\parallel}{\partial U} \right)_\phi, \quad (54)$$

and the partial derivatives of $T = T(\phi, U)$ and $T_\parallel = T_\parallel(\phi, U)$ can be evaluated using the algebraic energy balances (50). The dispersion relationship takes the form

$$\phi_0 \alpha^2 + \left[\frac{\phi_0 R_{\text{drag}}}{St} + ik \left(\frac{\partial P_m}{\partial U} \right)_\phi + \mu_c k^2 \right] \alpha - ik \phi_0^2 \frac{R'_{\text{drag}}}{St R_{\text{drag}}} + k^2 \phi_0 \left(\frac{\partial P_m}{\partial \phi} \right)_U = 0. \quad (55)$$

Substituting (49) into (55), we obtain a kinematic wave speed:

$$-\sigma_1 = U_0 - \frac{R'_{\text{drag}} \phi_0}{R_{\text{drag}}^2} \quad (56)$$

and the growth rate for large wavelengths:

$$\sigma_2 = \frac{St}{R_{\text{drag}}} \left[\frac{\phi_0^2 (R'_{\text{drag}})^2}{R_{\text{drag}}^4} - \left(\frac{\partial P_m}{\partial \phi} \right)_U + \frac{R'_{\text{drag}}}{R_{\text{drag}}^2} \left(\frac{\partial P_m}{\partial U} \right)_\phi \right]. \quad (57)$$

To confirm that this local energy balance formulation captured the correct long-wavelength behaviour, we performed a small- k asymptotic analysis on the dispersion equation resulting from the full problem and obtained the same results for σ_1 and σ_2 .

Since all suspensions with $\sigma_2 > 0$ are unstable and most cases with $\sigma_2 < 0$ are stable at all wavenumbers, (57) provides a condition that can be used to estimate the critical Stokes number above which the suspension is unstable. The first term on the right-hand side of (57) results from the particle inertia and the dependence of the drag on volume fraction. This is the same destabilizing term found in previous stability analyses (Jackson 1963). The second term indicates that the increase of pressure with increasing volume fraction tends to stabilize the suspension by driving a flow from dense regions to dilute regions of the bed. This is similar to the stabilizing mechanism identified previously (Anderson & Jackson 1968). In previous analyses, the pressure was considered to be a function of the volume fraction alone and no energy balance was considered. In our analysis, the partial derivative of pressure with respect to volume fraction involves both a direct dependence and a contribution from the change in the particle temperature as determined by the local energy balance. An additional destabilizing term results from the dependence of the pressure on velocity. An increase in the mean velocity of the particles increases the source of energy due to hydrodynamic interactions and thereby increases the particle temperature and pressure. This tends to drive particles from dilute regions with fast moving particles into dense regions with slow moving particles. This effect is not incorporated in

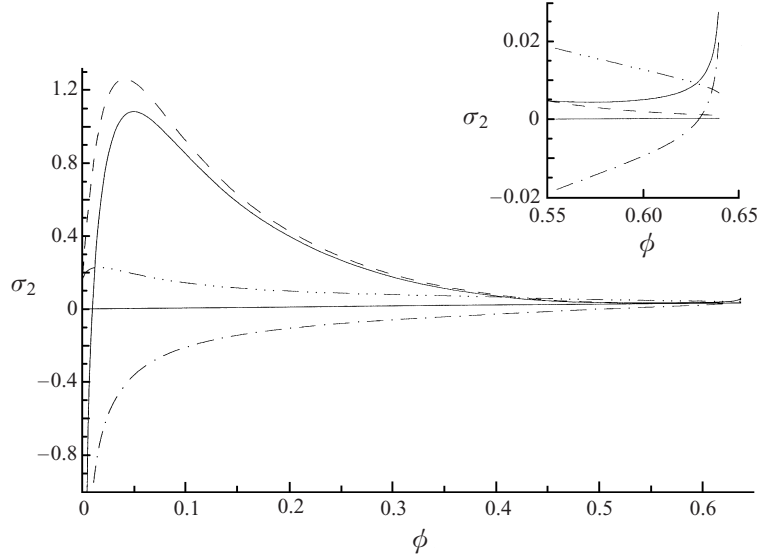


FIGURE 10. The leading real contribution to the growth rate in the limit of small wavenumber, σ_2 , plotted as a function of the particle volume fraction is indicated by the solid curve. The dashed, dash-dot and dash-dot-dot curves indicate the first, second and third contributions defined in (57). The Stokes number is 50 and the coefficient of restitution is 1.

previous studies which assumed no dependence of the particle pressure on relative velocity.

The contributions of these three terms to σ_2 are illustrated in figure 10 for perfectly elastic particles with $St = 50$ and a range of volume fractions. The destabilizing term resulting from the dependence of R_{drag} on volume fraction (term 1, dashed line) is zero at $\phi = 0$, grows rapidly with ϕ , passes through a maximum at $\phi = 0.046$, and decreases at higher volume fractions.

The destabilizing term due to the dependence of particle pressure on U (term 3, dash-dot-dot line) shows a similar behaviour but with a smaller amplitude. Thus, the traditional destabilizing term is still the most significant one. The resistance of the suspension to compression, i.e. $-\partial P_m / \partial \phi$ (term 2, dash-dot line) is negative and provides a small window of stability at low volume fractions $\phi < 0.0125$. However, this stabilizing effect is diminished at higher volume fractions. In fact, $-\partial P_m / \partial \phi$ actually becomes positive for $\phi > 0.575$. As illustrated previously in figures 6 and 7, the particle pressure decreases with increasing ϕ in very dense beds. This occurs because the increased viscous dissipation and decreased source of fluctuation energy lead to a diminution of the particle temperature as one approaches the close-packed limit. The destabilizing effect of this negative compressibility leads to a 6.5-fold increase in σ_2 between $\phi = 0.575$ and 0.64 (see insert of figure 10).

The critical Stokes number above which the homogeneous unbounded suspension is unstable is plotted as a function of volume fraction for several values of the coefficient of restitution in figure 11. In the dilute limit, the critical Stokes number is $0.149\phi^{-3/2}$. However, this dilute asymptote is only quantitatively accurate (relative errors of less than 5%) for volume fractions less than 0.001. For values of ϕ greater than about 0.05, the critical Stokes number for an unbounded suspension is sufficiently small, $St_c < 5$, that the high-Stokes-number theory is not applicable. Thus, except in the dilute limit, an unbounded, high-Stokes-number suspension undergoing

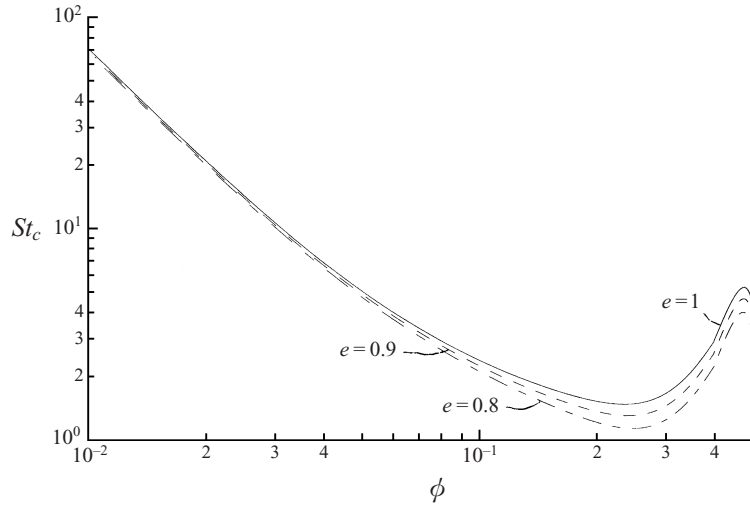


FIGURE 11. The approximation to the critical Stokes number obtained by setting σ_2 equal to zero is plotted as a function of the volume fraction for $e = 1$ (solid line), 0.9, and 0.8 (dashed lines).

hydrodynamic interactions and short-duration solid-body collisions is unstable. This observation is consistent with the experimental observation of Tsinotides & Jackson (1993) that frictional forces are associated with the interval of stable fluidization in the gas-fluidized beds examined in their experimental studies.

It is interesting to note that the critical Stokes number for elastic particles passes through a minimum of 1.41 at $\phi = 0.237$ and a maximum of 4.98 at $\phi = 0.479$ before diminishing once again. Over a small range of volume fractions, $0.518 < \phi < 0.52$, the theory predicts an unstable suspension at low Stokes numbers followed by a narrow window of stability and an unstable suspension at high Stokes numbers. Above $\phi = 0.52$, the suspension is unstable at all Stokes numbers. However, it should be noted that the details of the behaviour of $St_c(\phi)$ in dense suspensions may not have physical significance because the high-Stokes-number theory is not applicable at the low-to-moderate Stokes numbers at which the marginal stability limit occurs. Therefore, the main conclusion that can be drawn is that high-Stokes-number suspensions are unstable.

Most analyses of gas-fluidized beds, other gas-solid suspensions, and granular flows assume that the particle velocity fluctuations are nearly isotropic. In the present theory, we have adopted separate energy balances for the vertical and horizontal velocity fluctuations with an energy exchange between these modes resulting from solid-body collisions. We found that the velocity variance exhibits substantial anisotropy owing to the larger source of fluctuating energy in the vertical direction, cf. figure 4. It is interesting then to examine the effect that the anisotropy of the velocity variance has on the stability predictions by comparing the results for the full analysis with those for a simplified analysis based on a single overall energy balance. This comparison is given in figure 12 where the critical Stokes number is plotted as a function of ϕ . The theory based on an isotropic velocity variance gives $St_c \sim 0.0788/\phi^{3/2}$ in the limit $\phi \rightarrow 0$ in agreement with the asymptotic analysis of Koch (1990). This dilute suspension behaviour is similar to that obtained from the full anisotropic variance calculations but St_c is decreased by a factor of about 2. The anisotropic theory takes into account the fact that most of the energy is contained in vertical velocity

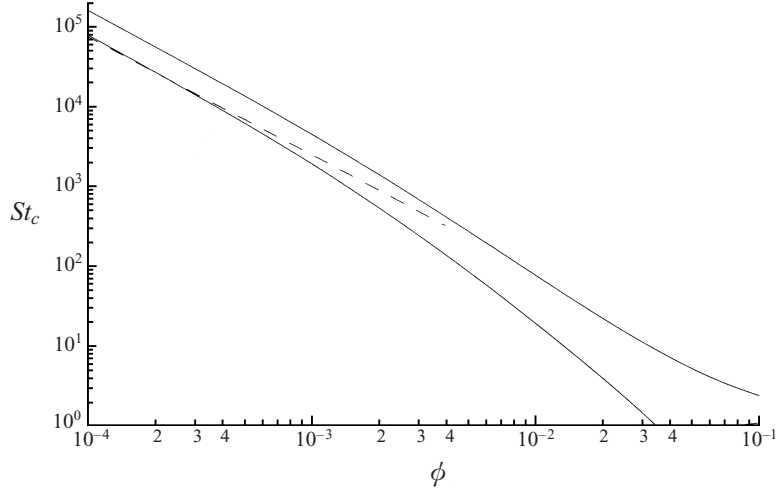


FIGURE 12. The approximate critical Stokes number for perfectly elastic particles obtained from the full theory (upper solid curve) is compared with that obtained from a model with an isotropic granular temperature (lower solid curve). The dashed line is the dilute asymptote $0.0788 St/\phi^{3/2}$ for an isotropic suspension derived by Koch (1990).

fluctuations and it is these fluctuations that tend to stabilize the suspension to vertical waves. The critical Stokes number obtained for an isotropic granular temperature goes to zero at $\phi = 0.0794$, whereas the anisotropic-variance analysis gives a small but finite St_c in more concentrated suspensions.

When numerical simulations are performed in a unit cell with periodic boundary conditions, this will restrict the wavelength of the disturbances that can affect the system. The stability analysis predicts a minimum wavelength (maximum wavenumber) for instability at any $St > St_c$ as illustrated in figures 8 and 9. In practice, we have found that a periodic unit cell that is large enough to contain enough particles to approximate a continuum will be large enough to admit unstable modes except at Stokes numbers that are very close to the critical value. For example, for $\phi = 0.02$ and $St = 22$ (close to the critical Stokes number of 16–17), the maximum unstable wavenumber $k = 0.42$ corresponds to a cubic unit cell containing 15 particles.

The plots of growth rate as a function of wavenumber in figures 8 and 9 show that the growth rate passes through a maximum at an intermediate value of the wavenumber. In figure 13, we present the maximum growth rate σ_m as a function of volume fraction for perfectly elastic particles at $St = 5, 10, 50$, and 100 . In very dilute suspensions, the maximum growth rate is zero and the suspension is stable. As the volume fraction increases, σ_m grows, passes through a maximum at $\phi \approx 0.1$ and decreases again. The maximum growth rate becomes quite small ($\sigma_m = O(10^{-3})$) for $\phi \approx 0.45$ – 0.55 . This suggests the possibility that the instability of a fluidized bed could be missed in numerical integrations of the equations of motion if insufficient time is allowed for the perturbations to grow. However, it should be noted that the dimensional growth rate remains sufficiently high that the instability would be readily observed in experiments. For example, the dimensional growth rate for the most dangerous mode for $60 \mu\text{m}$ diameter particles with density of 1 g cm^{-3} at atmospheric conditions would always be greater than 1.4 s^{-1} . The dimensional wave speed under these conditions is about 0.8 cm s^{-1} , so that the disturbance would only propagate

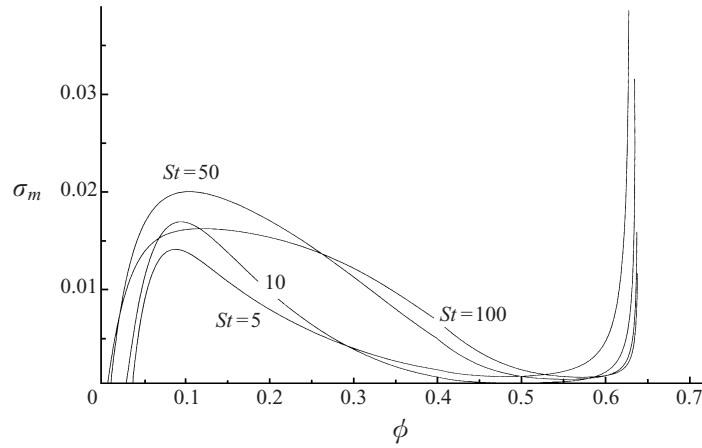


FIGURE 13. The maximum growth rate of waves in an unbounded suspension is plotted as a function of the volume fraction for perfectly elastic particles with $St = 5, 10, 50$, and 100 .

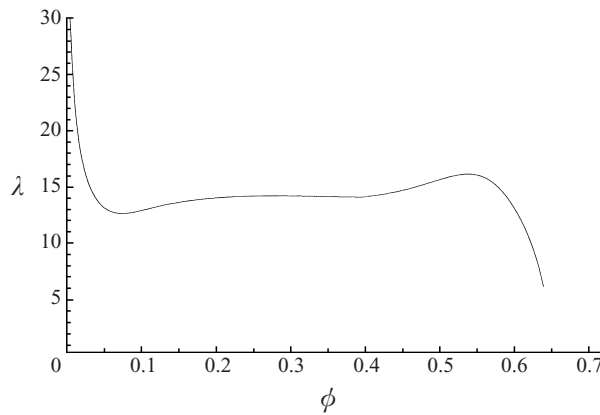


FIGURE 14. The wavelength λ of the fastest growing instability non-dimensionalized by the particle radius is plotted as a function of volume fraction for $St = 100$.

about 1 cm while increasing in amplitude by a factor of e . Comparing figures 10 and 13, it may be seen that the qualitative dependence of the maximum growth rate on volume fraction mirrors the behaviour of the growth rate in the long-wavelength limit. The wavelength of the fastest growing wave non-dimensionalized by the particle radius is plotted as a function of ϕ for $St = 100$ in figure 14. The wavelength is very large in dilute suspensions and approaches infinity at the critical volume fraction for instability. At moderate volume fractions, the wavelength is about 10–15 times the particle radius. This value is somewhat smaller than the wavelength (about $40a$) of the void fraction waves observed in liquid-fluidized beds by Didwania & Homsy (1981).

The maximum growth rate increases rapidly with volume fraction for very dense suspensions, $0.57 < \phi < 0.64$, cf. figure 13. This sharp increase coincides with the regime in which the particle pressure decreases with increasing volume fraction so that the suspension is mechanically unstable even in the absence of a volume-fraction-dependent mean drag coefficient. It should be noted that the high growth rates

St	$U_t t/a$	T_{\parallel}/U_t^2	T_{\perp}/U_t^2	U/U_t	Θ_{\parallel}	Θ_{\perp}	$g(2.1a)$
0	3000	0.0534	0.0038	0.747	1.00	0.91	2.23
2	4000	0.0517	0.0039	0.748	1.04	1.07	2.12
5	4000	0.0633	0.0035	0.790	1.09	1.06	3.54
20	5000	0.0485	0.0020	0.766	1.05	1.17	3.18
50	10000	0.0313	0.0012	0.729	1.09	0.99	2.39
100	10000	0.0183	0.0010	0.717	1.03	1.14	1.75
200	15000	0.0090	0.0007	0.697	0.97	0.84	1.25
350	15000	0.0051	0.0006	0.692	1.05	0.94	1.33
50	20000	0.0031	0.0005	0.681	0.98	0.88	1.03
750	25000	0.0026	0.0004	0.678	1.05	0.85	1.00

TABLE 4. Dynamic simulation results for $\phi = 0.02$ with $N = 16$. t is the time interval used for computing the average properties.

predicted for $\phi > 0.57$ may not be obtained in practice because of the inapplicability of the assumed form of the equations of motion at these high concentrations. Dense suspensions may exhibit a solid-like behaviour when there is insufficient free volume to allow the particles to translate relative to one another. Deviations of the behaviour of dynamical simulations of hard spheres from the predictions of the kinetic theory for dense gases are typically observed for $\phi > 0.55$ (Woodcock 1981).

5. Dynamic simulations

In the previous sections, we presented equations of motion for a gas-fluidized bed and examined their linear stability. The source of particle fluctuation energy arising due to the particles' motion relative to the gas was computed using simulations of interparticle hydrodynamic interactions that approximated the particle motions as those in a homogeneous hard-sphere system. In the present section, we will discuss results of dynamic simulations obtained by solving the full equations of motion for the particles and the viscous gas. These simulations will be used to test certain aspects of the theoretical predictions of particle temperature and the instability of a homogeneous gas-fluidized bed. The simulations for systems with fewer than $N = 64$ particles were conducted using the method described in Sangani & Mo (1994) and Sangani *et al.* (1996) while those for larger systems were based on the $O(N)$ algorithm described in Sangani & Mo (1996) with a few modifications to be specified later in this section. All of the simulations used a lubrication cut-off of $\epsilon_m = 0.01$ to account for the finite mean-free path of the interstitial gas.

Results for the velocity variance as a function of St in a dilute suspension with $\phi = 0.02$ and $N = 16$ were presented earlier in figure 3. A more detailed account of these simulations is given in table 4. The initial condition for each simulation was specified as a hard-sphere spatial distribution with each particle's velocity equal to the steady-state mean sedimentation velocity. The equations of motion for the hydrodynamically interacting particles were then solved for several thousand Stokes settling times a/U_t to reach a statistical steady state. Thereafter, the simulations were run for the times specified in table 4 and time-average properties of the suspension were computed.

Two measures of the spatial configuration of the particles were monitored. The value of the radial distribution function $g(r)$ at $r = 2.1a$ was used to quantify short-

range clustering tendencies. As noted previously (Ladd 1996; Koch & Shaqfeh 1991), the probability of close pairs in a dilute sedimenting suspension without particle inertia is higher than that in a hard-sphere fluid. As the Stokes number is increased to $St = O(10)$, particle inertia allows particles to come closer to one another and the tendency for small-scale clustering increases. At higher Stokes numbers, however, particles have sufficient inertia to bounce off one another and separate after a collision and $g(2.1a)$ decreases and approaches the hard-sphere value. The small-scale clustering at moderate St results in an increase in the mean sedimentation velocity because two spheres in close proximity fall faster than a single sphere. As the Stokes number is increased further, the mean velocity passes through a maximum and decreases as a result of the decreased probability of close pairs. The stronger (fixed-bed-like) hydrodynamic interactions between high-Stokes-number particles also decrease the mean velocity. For $St \geq 500$, the simulated mean velocities are comparable with the value $0.683U_t$ obtained for a fixed bed, cf. (19).

The second measure of spatial configurations is the structure factor defined by

$$S(\mathbf{k}) = \left\langle \frac{1}{N} \sum_{\alpha=1}^N \sum_{\gamma=1}^N \exp(2\pi i \mathbf{k} \cdot (\mathbf{x}^\alpha - \mathbf{x}^\gamma)) \right\rangle. \quad (58)$$

This is used to quantify microstructural changes occurring on the lengthscale of the periodic box used in the simulations. In particular, since the instability is predicted to occur first for the largest wavelength possible, the structure factors

$$\Theta_{\parallel} = S(\mathbf{e}_z/H), \quad \Theta_{\perp} = [S(\mathbf{e}_x/H) + S(\mathbf{e}_y/H)]/2 \quad (59)$$

corresponding to the smallest vertical and horizontal wavenumbers (largest wavelengths) that fit in the box are reported in table 4. For hard-sphere systems with $\phi = 0.02$ and $N = 16$ these structure factors are approximately equal to 0.85. We see that the structure factors for finite-Stokes-number suspensions are comparable in magnitude: variations seen in table 4 are statistically insignificant. The stability analysis predicts that the homogeneous suspension is unstable for the cases with $St > 17$ listed in table 4. However, the box length is smaller than the mean-free path for the small number of particles (16) used in the simulations and the continuum description of volume fraction variations is inapplicable. These small boxes provide a means of approximating the behaviour of a homogeneous suspension and it was shown in figures 3 and 4 that the velocity variance obtained in the dynamic simulations was in agreement with the theory.

To find evidence of the inhomogeneity induced by the predicted instability, we performed a series of simulations (summarized in table 5a) with $St = 50$, $\phi = 0.05$ and a range of simulation cell sizes $N = 16$ –512. The theory predicts that the homogeneous suspension is unstable for these conditions. The structure factor for a homogeneous hard-sphere distribution is about 0.7 and is nearly independent of N . The structure factors obtained from the dynamic simulations grow with increasing box size and are consistently higher than those for a hard-sphere distribution. This is illustrated in figure 15(a) where the vertical and horizontal structure factors are plotted as circles and squares, respectively, and the structure factor for a hard-sphere distribution is indicated by the triangles. In the largest unit cells $N = 512$, the structure factor is 2–4. The structure factor may be expected to grow with N if the structure consists of a macroscopic inhomogeneity rather than local particle-scale clustering. The inhomogeneous structure leads to a spatially varying gravitational

	N	tU_t/a	T_{\parallel}	T_{\perp}	U/U_t	Θ_{\parallel}	Θ_{\perp}	Θ_{HS}
(a)	16	2500	0.027	0.0018	0.573	1.06	0.80	0.73
	32	2500	0.035	0.0022	0.597	1.25	0.92	0.78
	64	4300	0.039	0.0035	0.594	1.01	1.04	0.66
	128	3900	0.045	0.0051	0.611	1.38	1.19	0.76
	256	3300	0.074	0.007	0.636	1.57	1.83	0.59
	512	520	0.084	0.008	0.659	2.13	3.50	0.69
(b)	9	600	6.9×10^{-4}	2.5×10^{-4}	0.083	0.44	0.22	0.10
	16	400	1.3×10^{-3}	3.0×10^{-4}	0.089	0.36	0.19	0.08
	32	800	1.6×10^{-3}	3.6×10^{-4}	0.086	0.88	0.23	0.08
	64	900	1.5×10^{-3}	6.5×10^{-4}	0.083	0.51	0.19	0.07
	1024	350	2.6×10^{-3}	9.3×10^{-4}	0.095	1.29	0.38	0.09

TABLE 5. Dynamic simulation results for (a) $St = 50$ and $\phi = 0.05$ and (b) $St = 100$ and $\phi = 0.35$ as a function of N . Θ_{HS} is the structure factor for the hard-sphere systems. Note that the simulation for $N = 512$ in (a) was carried out for a relatively short period and therefore the results for that case may not represent steady-state values.

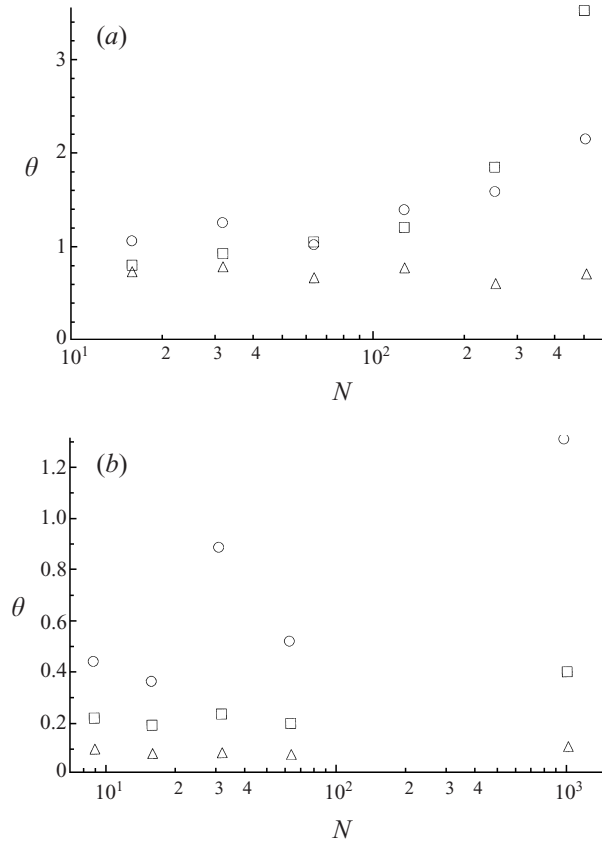


FIGURE 15. The box-length structure factors Θ_{\parallel} (circles) and Θ_{\perp} (squares) for gas–solid suspensions with (a) $\phi = 0.05$ and $St = 50$ and (b) $\phi = 0.35$ and $St = 100$. The triangles correspond to Θ_{\parallel} for a hard-sphere system with the same N and ϕ .

force that drives velocity fluctuations in the suspension. These are seen in the form of a velocity variance in the vertical direction that grows from 0.027 for $N = 16$ to 0.084 for $N = 512$. For comparison, the velocity variance predicted for a homogeneous suspension is 0.0129.

It is likely that the enhanced particle pressure created by the shear work associated with this macroscopic shearing motion limits the extent of the suspension structure formed. The mean velocity of the particles also grows with box size. This may be attributed to the fact that more particles will be found in dense downward flowing portions of the suspension than in less dense regions with upward mean mixture velocities.

The simulations discussed above were performed with the multipole order for individual particles corresponding to $N_s = 2$. Large- N simulations using the $O(N)$ algorithm described in Sangani & Mo (1996) also require a specification of N_{sp} , the multipole order used in representing the far-field velocity induced by groups of particles. The results presented in table 5 for $N \geq 64$ employed $N_{sp} = 3$. Computations were also made with $N_{sp} = 4$ for somewhat smaller time duration to assess the effect of varying N_{sp} , and it was found that $N_{sp} = 3$ and $N_{sp} = 4$ gave essentially the same results.

Simulations for a more dense suspension ($\phi = 0.35$ and $St = 100$) that is predicted to exhibit inhomogeneous structure are summarized in table 5(b). Since the source of velocity fluctuations at $\phi = 0.35$ for $N_s = 2$ is much smaller than for $N_s = 3$, these simulations were made with $N_s = 3$. At higher volume fractions the error introduced by grouping the particles in the $O(N)$ algorithm is significant unless sufficiently large N_{sp} is used. For simulations with $N = 1024$ this required that $N_{sp} \geq 5$ be chosen to minimize the error. The computing time increases roughly as N_{sp}^4 , and therefore $N_{sp} = 5$ requires about 35 times more computing time than the value $N_{sp} = 2$ used in Sangani & Mo (1996). In that study, the same N_{sp} was used for groups of different sizes. We found that the computing time can be reduced significantly without sacrificing accuracy if a smaller N_{sp} was used for smaller groups of particles and a larger N_{sp} for larger groups. Thus, the results for $N = 1024$ were obtained by using N_{sp} of 4 for level 2 particle groups and N_{sp} of 5 for level 1 groups.

The results for $\phi = 0.35$ are similar to those for $\phi = 0.05$. The box-length structure factor reaches a value of 0.4–1.3 at $N = 1024$ that is much higher than the value (0.1) for a hard-sphere distribution. This is illustrated in figure 15(b) where the parallel and perpendicular structure factors for the suspension are plotted as circles and squares respectively and the hard-sphere structure factor is given by the triangles. An alternative way of visualizing the suspension structure is to divide the simulation cell for $N = 1024$ into 64 boxes so that on average each box contains 16 particles. The variation of the mean volume fraction among these boxes then gives an indication of the inhomogeneity of the suspension and the tendency to form regions devoid of particles which may represent the first stages of bubble formation. The minimum and maximum volume fractions ϕ_{min} and ϕ_{max} among the boxes is plotted as a function of time in figure 16 for the gas-fluidized bed (lines) and a hard-sphere system with the same $T_{||}$ (plusses and crosses). The smallest ϕ_{min} attained in the gas–solid suspension correspond to 6 particles in a box whereas the most dilute regions for the hard-sphere system contained 10 particles. As in the more dilute suspensions, the velocity variance at $\phi = 0.35$ increases with increasing system size. The variance grows from a value $T = 6.3 \times 10^{-4}$ at $N = 16$ that is 40% higher than that for a homogeneous suspension to a value $T = 1.5 \times 10^{-3}$ for $N = 1024$ that is more than three times larger than the homogeneous value.

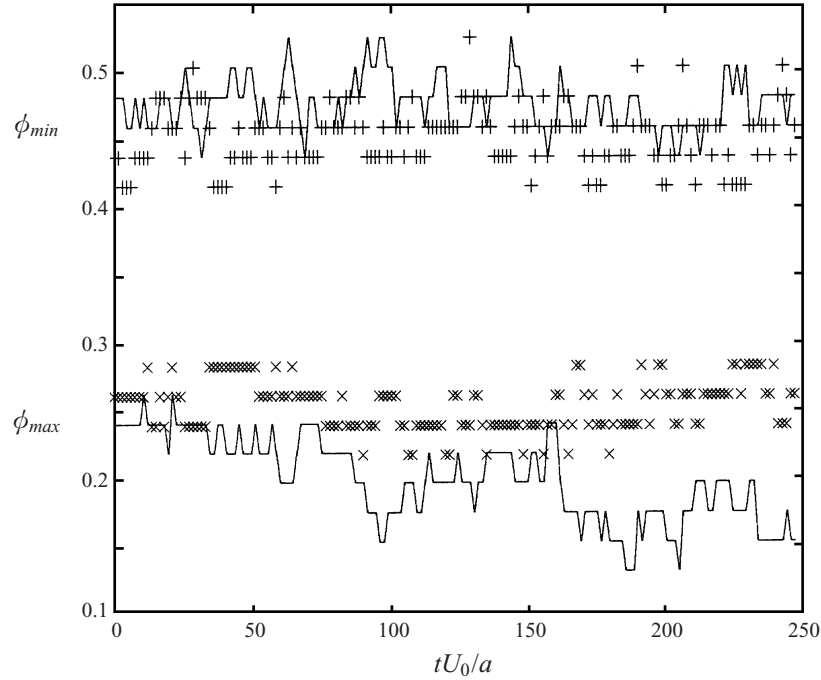


FIGURE 16. ϕ_{min} and ϕ_{max} as a function of time for a simulation with $N = 1024$ and $\phi = 0.35$. The solid lines represent sedimenting suspensions with $St = 100$ and the plusses and the crosses represent a hard-sphere system with the same value of T_{\parallel} .

6. Conclusions

In this paper, we have derived equations of motion for gas–solid suspensions with a mean relative motion between the gas and particulate phases. The equations presented in §4 apply when all the spatial gradients are parallel to gravity. A more complete set of equations of motion allowing for arbitrary spatial gradients is summarized in the Appendix. The theory of rapid granular flows as derived, for example, by Lun *et al.* (1984) describes the flow of particles in a vacuum by incorporating inelastic particle collisions in the theory of dense gases. Sangani *et al.* (1996) extended this work to sheared gas–solid suspensions by determining the viscous dissipation of energy. Here, we have generalized the work of Sangani *et al.* to allow for a mean relative motion of the two phases. This relative motion gives rise to a mean drag force which, for a high-Stokes-number suspension, is equivalent to that acting on a fixed bed of particles, cf. figure 2 and (26). In addition, the fluctuating gas velocity field produced by the mean motion of the randomly positioned particles exerts fluctuating forces on the particles that result in a source of particulate-phase fluctuating energy given by (22) and (23) and figure 1. The present theory like those of Lun *et al.* and Sangani *et al.* assumes that the particles undergo instantaneous solid-body collisions but do not experience enduring solid-body contacts.

As applications of these equations of motion, we calculated the particle velocity variance (or granular temperature) and particle pressure in a homogeneous sedimenting gas–solid suspension or gas-fluidized bed and determined the marginal stability limits of the homogeneous state. The theoretical results were compared with dynamical simulations that solved the detailed equations of motion for an array of $N = 16$ – 1024 particles in a viscous gas. At moderate-to-high Stokes numbers, the velocity variance

non-dimensionalized by the square of the particles' terminal velocity decays like $St^{-2/3}$ with increasing Stokes number as illustrated in figure 3. The sedimenting particles produce stronger velocity fluctuations in the vertical than the horizontal direction and this makes the source of fluctuating energy highly anisotropic. As a result, the vertical velocity variance is significantly higher than the horizontal except at very high Stokes numbers where the solid-body collisions can efficiently transfer energy from vertical to horizontal motions, cf. figure 4.

The particle pressure (presented in figures 6 and 7) grows at first with increasing volume fraction due to the increasing particle concentration and the higher frequency of interparticle collisions. However, this growth is slower than would be obtained for a constant-temperature molecular gas because the temperature in the gas-solid suspension decreases with increasing volume fraction. This decreased temperature arises because of the stronger viscous dissipation occurring in a dense suspension and because the hydrodynamic source of energy decreases with increasing volume fraction. In very dense suspensions, $\phi > 0.57$, the particle pressure actually decreases with increasing volume fraction.

Prediction of the marginal stability limits for the homogeneous state of a gas-fluidized bed has long been considered an important test for proposed equations of motion for particulate flows. The standard theory identifies the coupled effects of particle inertia and the dependence of the drag coefficient on volume fraction as the destabilizing mechanism, while the particle-phase pressure was supposed to stabilize the homogeneous suspension under certain conditions. However, up to the present time, there has been no rigorous derivation of the magnitude of the particle-phase pressure and so a predictive theory for the marginal stability limits could not be obtained. We have carried this line of theoretical investigation to its logical conclusion by using kinetic theory and Stokes flow simulation methods to derive the particle-phase pressure and rheology in a gas-solid suspension over a wide range of particle volume fractions and Stokes numbers. An important part of this derivation is the determination of the particle-phase velocity variance tensor including hydrodynamic sources and sinks of particle-phase fluctuating energy. Thus, the equations of motion in the present investigation differ from those in much of the previous fluidized-bed literature in that they incorporate explicit energy equations for the vertical and horizontal particle velocity fluctuations. The linear stability analysis of the resulting equations of motion indicates that the homogeneous state is unstable to vertical waves for Stokes numbers greater than about 5 except in very dilute suspensions, where the critical Stokes number is proportional to $\phi^{-3/2}$, cf. figure 11. This prediction is corroborated by our dynamic simulations which exhibit substantial deviations from the hard-sphere structure factor whenever the periodic unit cell is sufficiently large to admit waves that can be described by the continuum equations of motion for the suspension. The simulations also exhibit a velocity variance that grows with the simulation cell size; this variance may be attributed to the macroscopic shearing motions induced by the inhomogeneous particle distribution. Therefore, we conclude that the homogeneous state of a high-Stokes-number, dense, gas-fluidized bed is always unstable under circumstances in which the suspension may be described as a 'fluid' obeying equations of motion that can be derived on the basis of a microscale description of particles interacting via instantaneous hard-sphere collisions and hydrodynamic interactions.

This finding is consistent with the conclusion drawn by Tsinotides & Jackson (1993) based on their experimental observations that the homogeneous state of many (and possibly all) dense gas-fluidized beds is associated with a solid-like state of the

suspension. To gain a better understanding of this phenomenon, it would be desirable to formulate a theoretical description of the transition from the solid-like behaviour that must occur in the dense-packed limit and the fluid state described in the present work.

It may be difficult to obtain a direct experimental test of our theoretical predictions beyond the observation that high-Stokes-number, dense, fluid-like gas-fluidized beds are unstable. A typical system of 70 μm diameter particles with a density of 2.5 g cm^{-3} has a Stokes number of 400. Thus, a homogeneous suspension of these particles would only be expected to be stable if it were very dilute $\phi < 0.004$. To observe this marginal stability limit, great care would need to be taken to ensure that the suspension is initially well mixed so that any observed inhomogeneities can be attributed exclusively to inherent instabilities of the suspension. The marginal stability limits for high volume fractions are not of practical relevance to terrestrial gas–solid suspensions, because any particles small enough to exhibit the small Stokes numbers required would also be affected by electrostatic, van der Waals, and/or Brownian forces. It may be possible to produce a moderate-Stokes-number gas–solid suspension interacting via collisional and hydrodynamic forces by using large particles under microgravity conditions. A less exotic system that can exhibit Stokes numbers in the range 1–10 is a suspension of particles fluidized by a viscous liquid. The present theory is not directly applicable to this situation because it neglects the inertia of the fluid (in a liquid–solid system the Stokes and Reynolds numbers are comparable in value). In addition, the quantitative accuracy of the high-Stokes-number theory is questionable for $St = 1$ –10. Nonetheless, the present work may elucidate some of the relevant physical considerations governing the stability of such a system.

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Appendix. Equations of motion for a sheared gas–solid suspension with relative motion between the phases

In §4, we presented equations of motion for a gas–solid suspension obtained by generalizing the analysis of Sangani *et al.* (1996) to allow for a relative motion of the gas and solid phases. Because we were interested in the behaviour of particle volume fraction waves with spatial variations parallel to the direction of the mean flow, we simplified the equations for this special case. In this Appendix, the full equations of motion for a gas–solid suspension with relative velocity between the phases and spatial gradients of velocity and volume fraction in arbitrary directions will be summarized. These consist of mass and momentum conservation equations for the gas and solid phases and an equation for the second moment of the particle velocity.

The mass conservation equations for the particle and gas phases are

$$\frac{\partial \phi}{\partial t} + \nabla \cdot (U\phi) = 0 \quad (\text{A } 1)$$

$$\frac{\partial (1 - \phi)}{\partial t} + \nabla \cdot [V(1 - \phi)] = 0, \quad (\text{A } 2)$$

where \mathbf{V} is the mean velocity of the gas phase. Alternatively, one can consider the mixture average velocity $\mathbf{W} = \mathbf{V}(1 - \phi) + \phi\mathbf{U}$ as a dependent variable in place of \mathbf{V} . The incompressibility of the mixture implies that

$$\nabla \cdot \mathbf{W} = 0. \quad (\text{A } 3)$$

The particle momentum conservation equation obtained from (4.13)–(4.16) and (4.22) of Sangani *et al.* (1996) takes the form

$$\rho_p \phi \left(\frac{\partial \mathbf{U}}{\partial t} + \mathbf{U} \cdot \nabla \mathbf{U} \right) = \rho_p \phi \mathbf{g} + 6\pi\mu a n(1 - \phi) R_{\text{drag}}(\mathbf{V} - \mathbf{U}) + \nabla \cdot \boldsymbol{\sigma} \quad (\text{A } 4)$$

where R_{drag} is given by (25) and (26). In §§ 3 and 4, it was assumed that the mixture velocity was zero and the drag force was then expressed solely in terms of the particle velocity. Here, we have written the drag in terms of the difference between the particle and gas velocities, so that (A 4) can be applied to the case $\mathbf{W} \neq 0$. The particle stress is related to the second moment T_{ij} of the particle velocity by

$$\sigma_{ij} = -\rho_p \left(\phi + \frac{8}{5}B \right) T_{ij} - \frac{12}{5}\rho_p B T \delta_{ij} + \frac{32}{5\pi^{1/2}}\rho_p B a T^{1/2} (e_{ij} + \frac{1}{2}e_{kk}\delta_{ij}) \quad (\text{A } 5)$$

where B is given by (41) and the rate of strain is

$$e_{ij} = \frac{1}{2} \left(\frac{\partial U_i}{\partial x_j} + \frac{\partial U_j}{\partial x_i} \right). \quad (\text{A } 6)$$

Because the density of the gas is much smaller than that of the particles, we will neglect the inertia of the gas and approximate the gas momentum equation as a balance of the gradient of the gas pressure p , the force per unit volume exerted by the particles on the gas, and the viscous stresses in the gas:

$$\nabla p = 6\pi\mu a n(1 - \phi) R_{\text{drag}}(\mathbf{U} - \mathbf{V}) + \mu \nabla^2 \mathbf{V}. \quad (\text{A } 7)$$

In writing (A 7) we have neglected any effect of the particles on the gas-phase viscous stress. This effect will be $O(\phi)$ in the dilute limit. In more concentrated suspensions, the viscous stress in the gas may be neglected compared with the drag force provided that the gas velocity varies over a lengthscale large compared with the particle diameter.

Finally, the equation for the second moment of the particle velocity obtained by supplementing equations (4.8), (4.10), (4.21), and (4.22) of Sangani *et al.* (1996) with the hydrodynamic source of energy computed in § 3 of the present paper takes the form

$$\begin{aligned} \frac{1}{2}\phi \left(\frac{\partial T_{ij}}{\partial t} + U_k \frac{\partial T_{ij}}{\partial x_k} \right) &= \frac{\partial}{\partial x_k} \left(a\kappa \frac{\partial T_{ij}}{\partial x_k} \right) - \left[\phi + \frac{4}{5}B(6\eta - 4) \right] T e_{ij} \\ &\quad - \frac{\mu_c}{a} \left[(2 - \eta) T_{ij} - \left(\frac{1}{3} + \frac{2}{3}\eta \right) T \delta_{ij} \right] - 2 \left(\phi + \frac{8}{5}B \right) e_{jk} (T_{ki} - T \delta_{ki}) \\ &\quad - \frac{\phi}{\tau_v} R_{\text{diss}} T_{ij} + \frac{\mu_c a}{3} \left[\frac{\partial U_i}{\partial x_k} e_{jk} + \frac{\partial U_j}{\partial x_k} e_{ki} + e_{kk} e_{ij} \right] - \frac{12}{5}B \left(\eta - \frac{2}{3} \right) e_{kk} \delta_{ij} T \\ &\quad + \frac{81\phi\mu^2}{4\rho_p^2 a_3 T^{1/2}} [S_{\perp}^* |\mathbf{U} - \mathbf{V}|^2 \delta_{ij} + (S_{\parallel}^* - S_{\perp}^*)(U_i - V_i)(U_j - V_j)] \end{aligned} \quad (\text{A } 8)$$

where $\tau_v = m/(6\pi\mu a)$ is the viscous relaxation time for the particle velocity, μ_c is given by (40), the sources S_{\parallel}^* and S_{\perp}^* may be obtained from (32) and (33), and the dependence of R_{diss} and R_s on volume fraction are expressed in (27) and (23). The non-dimensional thermal conductivity κ is given by (44). As noted in § 4, the

divergence of the third velocity moment arising in the equation for the second moment must be approximated to obtain a closed set of equations. We have adopted the assumption that the conductive transport of each second moment may be expressed using Fourier's law for a hard-sphere gas. In the application in §4 to void fraction waves we used T_{\parallel} in the expression for κ based on the insight that the gradients of granular temperature and the relevant flux of granular energy were directed parallel to gravity. In the more general situation, it may be more appropriate to approximate κ by using the isotropic temperature T (one third of the velocity variance) in (44).

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